SOA from limonene: role of NO$_3$ in its generation and degradation


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Abstract

The formation of organic nitrates and secondary organic aerosol (SOA) were monitored during the NO$_3$+limonene reaction in the atmosphere simulation chamber SAPHIR at Research Center Jülich. The 24-h run began in a purged, dry, particle-free chamber and comprised two injections of limonene and oxidants, such that the first experiment measured SOA yield in the absence of seed aerosol, and the second experiment yields in the presence of 10 µg m$^{-3}$ seed organic aerosol. After each injection, two separate increases in aerosol mass were observed, corresponding to sequential oxidation of the two limonene double bonds. Analysis of the measured NO$_3$, limonene, product nitrate concentrations, and aerosol properties provides mechanistic insight and constrains rate constants, branching ratios and vapor pressures of the products. The organic nitrate yield from NO$_3$+limonene is $\approx$30%. The SOA mass yield was observed to be 25–40%. The first injection is reproduced by a kinetic model. PMF analysis of the aerosol composition suggests that much of the aerosol mass results from combined oxidation by both O$_3$ and NO$_3$, e.g., oxidation of NO$_3$+limonene products by O$_3$. Further, later aerosol nitrate mass seems to derive from heterogeneous uptake of NO$_3$ onto unreacted aerosol alkene.

1 Introduction

Biogenic volatile organic compounds (BVOCs) make up a large fraction of gas-phase organic compounds emitted to the atmosphere: on a global scale, vegetation emissions of VOCs are an order of magnitude greater than those from petrochemicals (Guenther et al., 1995). Furthermore, in the atmosphere, many of these compounds are rapidly oxidized and likely to form condensable products (Griffin et al., 1999). Among these compounds, monoterpenes are known to be important sources of secondary organic aerosol (SOA) (Goldstein and Galbally, 2007; Eerdekens et al., 2009; Tunved et al., 2006; Slowik et al., 2010; Hallquist et al., 1999).
If NO$_3$-initiated aerosol formation from biogenic VOCs is a significant contribution to organic aerosol loading in the atmosphere, this would provide a potential resolution to a paradox noted in the SOA literature: $^{14}$C measurements show the carbon in organic aerosol to be primarily modern, which is characteristic of natural emissions, from urban (≈50%) to remote areas (80–100%) (Schichtel et al., 2008). However, aerosol loading in both urban and rural areas is observed to be correlated to aging in anthropogenic emissions plumes (de Gouw et al., 2005; Quinn et al., 2006; Weber et al., 2007). NO$_3$ produced BVOC SOA resolves the paradox by requiring both an anthropogenic oxidant “trigger” and biogenic VOC to form aerosol. This mechanism of SOA formation is expected to be most significant in forested areas downwind of urban centers or power plants, where NO$_x$ is high and biogenic VOCs are abundant (Pye et al., 2010). Because the nitrate radical is photolabile, this mechanism is also expected to be most important at night or within a shaded forest canopy.

Limonene is of interest as a representative BVOC both due to its high emission rate among monoterpenes (Sakulyanontvittaya et al., 2008) and its possession of two double bonds. These two reactive sites for oxidation give limonene a rapid and direct route to the types of low-vapor pressure oxidized products that are likely to form secondary organic aerosol. As a consequence, limonene may contribute disproportionately to total SOA relative to other terpenoids (Lane et al., 2008; Maksymiuk et al., 2009). Further, limonene’s frequent use in household cleaning products and air fresheners makes it a common source of indoor air pollution when its oxidation results in aerosol formation (Wainman et al., 2000). Aerosol formation from the reaction of NO$_3$ with limonene has been the subject of a previous chamber study (Spittler et al., 2006); in excess limonene and no O$_3$, organic nitrates were formed in high yield (67%), accompanied by immediate SOA formation.

Here we report chamber measurements and kinetic modeling of gas- and aerosol-phase chemistry during SOA formation initiated by the NO$_3$+limonene reaction under excess oxidants.
2 Experimental

2.1 Atmosphere simulation chamber SAPHIR

The experiment described below was conducted on the 16 and 17 of June 2007 in the atmospheric simulation chamber SAPHIR at Research Center Jülich as part of the intercomparison campaign of NO$_3$ (Dorn et al., 2010), N$_2$O$_5$ (Apodaca et al., 2010), and NO$_2$ (Fuchs et al., 2009) measurements. The SAPHIR chamber is a large (270 m$^3$) cylindrical chamber with double walls made from FEP film. It is equipped with an automated shuttering system to enable simulation of day or night conditions. The chamber and its operation during simulation experiments has been described in detail (e.g., Rohrer et al., 2005; Bohn and Zilken, 2005; Wegener et al., 2007). The chamber was used for large instrument intercomparison campaigns (e.g., Apel et al., 2008; Schlosser et al., 2009) and it was shown to serve as an excellent platform for multi-instrument experiments. Only a brief description of the chamber instruments and chamber operation is presented in the following.

The chamber has standard instrumentation for measurement of NO (chemiluminescence), NO$_x$, temperature, pressure, humidity, dilution flow, and O$_3$ (UV-absorption). However, during this experiment ozone concentrations were measured by chemiluminescence in a modified ECO Physics CLD AL 700 (Ridley et al., 1992). A GC-FID system (Perkin-Elmer) was used to verify the cleanness after purging and to follow the ethane concentration as an inert tracer of dilution. The limonene concentration was measured by Proton Transfer Reaction Mass Spectrometry (PTR-MS, IONICON, Austria; Lindinger et al., 1998).

Before the experiment, the chamber was purged overnight to ppt levels of nitrogen oxides, ozone, and hydrocarbons using a large flow 300 m$^3$/h of clean synthetic air (N$_2$, O$_2$, purity >99.9999%). During the experiment, the pressure was maintained at 30–50 hPa above ambient to prevent contamination. The slight overpressure was held by a smaller replenishment flow of the same synthetic air as used for flushing. During the entire experiment a fan provided fast mixing of constituents within the chamber. Due
to the replenishment flow of 10–15 m$^3$/h all gases were diluted by a rate of $\approx 4$–5.5%/h. The shutter system was closed throughout the experiment, keeping the chamber in darkness.

The trace gases (NO$_2$, ethane, and limonene) were added to the replenishment flow. Ozone ($\approx 5\%$) was produced by silent discharge in pure oxygen and injected into the chamber. Before the reaction started, 500 ppm of CO was added to the chamber in order to scavenge any OH formed.

### 2.2 NO$_3$, N$_2$O$_5$, and NO$_y$ measurements

During the intercomparison campaign several instruments measuring NO$_3$ and N$_2$O$_5$ concentrations were operated at SAPHIR (Dorn et al., 2010; Apodaca et al., 2010). Here we employ the data set from one of the instruments, the Cavity Ring-Down Spectrometer (CRDS) of the NOAA Earth System Research Lab team (Dube et al., 2006; Fuchs et al., 2008). None of the conclusions of this manuscript depend strongly on the choice of the NO$_3$+N$_2$O$_5$ measurement, as all measurements agreed to within 20%.

NO$_2$ was measured by laser-induced fluorescence (LIF) and total peroxynitrates ($\Sigma$PNs), total alkyl and multifunctional nitrates ($\Sigma$ANs), and nitric acid (HNO$_3$) were determined using thermal dissociation to NO$_2$ in heated quartz ovens held at different temperatures (“NO$_2$-TD-LIF”) (Thornton et al., 2000; Day et al., 2002). Details of this instrument are described in Wooldridge et al. (2010).

Briefly, the NO$_2$-TD-LIF instrument sampled at 3 standard liters per minute (slpm) from ca. 10 cm above the floor of the SAPHIR chamber through a Teflon PFA inlet (40 cm of 3.2 mm inner diameter tubing). A glass capillary orifice was used to reduce pressure, and the sample was split to four channels. In the ambient temperature channel NO$_2$ is detected. The other channels are held at 180 °C, 350 °C, and 600 °C, where $\Sigma$PNs, $\Sigma$ANs, and HNO$_3$ dissociate to yield NO$_2$. The mixing ratio of each class of nitrate is calculated from the difference in total NO$_2$ measured in adjacent temperature channels. We expect both gaseous and semivolatile aerosol-phase nitrates to dissociate completely, while thermally stable salts such as NaNO$_3$ will not be detected.
The NO$_2$ concentration in the reduced-pressure sample flow ($P \approx$1.5 Torr, 200 Pa) is detected by LIF. Here, we excite with a 408 nm continuous-wave diode laser at (8 mW, Toptica Photonics DL100) and collect filtered red-shifted fluorescence ($\lambda > 650$ nm) with a photomultiplier tube (PMT, Hamamatsu H7421-50) mounted at 90° to both the laser and sample flow. This instrument employed two detection cells, with detection limits of $\approx$90 ppt $10 \text{s}^{-1}$ for NO$_2$ and $\approx$250 ppt $10 \text{s}^{-1}$ for $\Sigma$PNs, $\Sigma$ANs, and HNO$_3$. The lower sensitivity for higher oxides accounts for noise associated with subtraction of the up to 40 ppb NO$_2$ present in these experiments. Detection limits for this instrument were calculated as described by Day et al. (2002).

2.3 AMS and other particle instrumentation

An aerosol mass spectrometer (Aerodyne TOF-AMS) was operated to measure the aerosol chemical composition. The AMS was connected to the SAPHIR chamber via a stainless steel tube to minimize losses in the sampling line. The AMS working principles and modes of operation are explained in detail elsewhere (Canagartna et al., 2007). In brief, an aerodynamic lens system at the instrument inlet is used to remove gas and supermicron particles from the sample flow, while submicron particles are impacted on a tungsten vaporizer which is held at $\approx$600 °C. The resulting vapors are ionized with 70 eV electron impact ionization. A time of flight mass spectrometer is used for high resolution analysis of the chemical composition of these ions.

For the extraction of chemically resolved mass concentrations of individual species the AMS raw data are typically evaluated with standard assumptions as described by Allan et al. (2004). In brief, this approach makes use of the reproducibility of mass spectral patterns of typical inorganic aerosol components such as ammonium, sulphate and nitrate. Subtracting from a measured mass spectrum the contributions of inorganic constituents and the contribution of gas phase sample, which is exclusively composed of N$_2$, O$_2$, H$_2$O and gases with mixing ratios in the ppm range, one obtains the mass spectrum of the organic aerosol. Due to the non-selective ionization with electron impact at 70 eV used in the AMS and the high fragmentation induced, further identification
of individual molecules in a complex organic component is not possible. However, positive matrix factorization can be employed to obtain information about different chemical species (see below). Furthermore the assumptions on inorganic aerosol fragmentation patterns can be tested explicitly and revised where necessary. Inorganic nitrate from e.g., \( \text{NH}_4\text{NO}_3 \) is detected as \( \text{NO}^+ \) (\( m/z \) 30) and \( \text{NO}^+_2 \) (\( m/z \) 46) with a typical ratio of \( \text{NO}^+_2:\text{NO}^+ \) of 0.35. In the W-mode (high mass resolution) of the TOF-AMS, possible interferences on mass to charge ratios 30 (e.g., \( \text{CH}_2\text{O}^+ \)) and 46 (e.g., \( \text{CH}_2\text{O}_2^+ \)) can be identified and accounted for in the further data evaluation. This option has been used for the experiments described here to derive the nitrate content and identity of the SOA. The quantification of the nitrate content of the SOA was performed based on calibrations with \( \text{NH}_4\text{NO}_3 \) aerosol. The observed ratio of \( \text{NO}^+_2:\text{NO}^+ \) for SOA was \( 0.15 \pm 0.02 \) which is considerably lower than 0.35 throughout the experiments indicating that the aerosol did not contain significant amounts of inorganic nitrate or nitric acid. Nitrate quantification was performed under the following assumptions: the collection efficiency of the aerosol was set to one, in agreement with previous studies on \( \text{NO}_3^+ + \beta\text{-pinene} \) (Fry et al., 2009) and \( \text{NO}_3^+ + \text{isoprene} \) (Rollins et al., 2009) SOA formation. The relative ionization efficiency (RIE) of the organics was set to 1.4 which is the standard value in AMS analysis, and the RIE of nitrate was set to 1, assuming organic nitrates are ionized equally efficiently to \( \text{NH}_4\text{NO}_3 \).

Aerosol number concentrations were measured with a Water Condensation Particle Counter (TSI WCPC model 3785). To determine aerosol wall loss rate, we use the loss rate determined by an exponential fit of the decay of CPC-measured aerosol number concentration after it has peaked 10 h into the experiment, after the second limonene injection. The peak concentration was 70 000 particles cm\(^{-3}\), after which decay was steady. This fit gives an effective aerosol loss rate of \( \approx 7 \times 10^{-5} \text{ s}^{-1} \), or an effective aerosol chamber lifetime of \( \approx 4 \text{ h} \).
3 Results

Figure 1 displays an overview of the NO$_3$+limonene experiment. All time axes are shown in hours since the beginning of the experiment, which commenced (hour 0) at 06:00 UTC on 16 July 2007. The experiment was initiated after the SAPHIR chamber had been purged overnight with clean, dry air. At 26 min into the experiment (06:26 UTC, label A in Fig. 1), 10 ppb of limonene was introduced to the chamber by adding the appropriate volume of liquid, along with 22 ppb of NO$_2$. Reactive chemistry was initiated approximately 2.5 h later (08:49 UTC, label B in Fig. 1) by the addition of NO$_2$ to bring the concentration up to 28 ppb along with 38 ppb of O$_3$. After this point, NO$_3$ and N$_2$O$_5$ are produced in the chamber by the following reactions:

\[
\text{NO}_2 + \text{O}_3 \rightarrow \text{NO}_3 + \text{O}_2 \quad (R1)
\]
\[
\text{NO}_3 + \text{NO}_2 \rightarrow \text{N}_2\text{O}_5 \quad (R2)
\]
\[
\text{N}_2\text{O}_5 \rightarrow \text{NO}_3 + \text{NO}_2 \quad (R3)
\]

The sum N$_2$O$_5$+NO$_3$ is the total NO$_3$ reservoir, because as NO$_3$ is depleted, N$_2$O$_5$ decomposes rapidly to replenish NO$_3$ (Reaction 3).

Both O$_3$ and NO$_3$ react with the limonene, resulting in complete consumption of limonene within 2.5 h. Gas- and aerosol-phase organic nitrates are formed immediately upon initiation of this reactive stage of the experiment, with aerosol-phase nitrates increasing markedly after oxidation of the second double bond (at approximately 5 h and 10 h for the two injections). The apparent negative alkyl nitrate observations after the first injection (around hour 3 of the experiment, Fig. 1 lower panel) are due to the subtractive measurement technique for $\Sigma$ANs. Both gas- and aerosol-phase organic nitrate concentrations continue to increase after the limonene is completely consumed. Little nitric acid ($\leq$2 ppb) was observed over this 24-h experiment. After the consumption of limonene, NO$_3$ and N$_2$O$_5$ are observed to gradually build up in the chamber, as NO$_2$ and O$_3$ continue to be present in high concentration.
Four hours following the complete consumption of limonene, the SAPHIR chamber, now containing $\approx 10 \mu g m^{-3}$ of “seed” organic aerosol, was re-charged, bringing the NO$_2$ concentration to 38 ppb and O$_3$ to 60 ppb, followed by addition of $\approx 10$ ppb of limonene (14:45 UTC, label C in Fig. 1). (Note: Although 10 ppb limonene was injected, a peak of only 7 ppb was observed due to slow mixing relative to rapid oxidation. Thermal dissociation of N$_2$O$_5$ gives an instantaneous source of NO$_3$, such that during these first minutes, oxidation is largely NO$_3$ driven.) We observed immediate and sustained production of organic nitrates and aerosol, with significantly higher ultimate yields of both, compared to those after the first injection. NO$_3$ and N$_2$O$_5$ concentrations were again observed to build up in the chamber after the limonene had been completely consumed. Then, approximately one hour into this buildup, NO$_3$ and N$_2$O$_5$ decrease again for several hours, corresponding to a period where the highest organic nitrate concentrations and highest aerosol mass were observed.

4 Analysis

4.1 Organic nitrate yield

The organic nitrate yields (=branching ratio of organic nitrate channel) after oxidation of the two double bonds in limonene are different. Following each injection of limonene, two time-separated sequential increases in organic nitrate concentration were observed: the first while the limonene concentration was decreasing, and the second after all limonene precursor had reacted away. Organic nitrate formation requires NO$_3$ reaction, as there is not any NO in the chamber to react with RO$_2$. During the second increase NO$_3$ may be oxidizing products of either the limonene+O$_3$ or the limonene+NO$_3$ reaction. In the first oxidation step, 34% of the limonene reacted with O$_3$, the remainder with NO$_3$.

We assume that the endocyclic bond reacts with NO$_3$ about thirty times faster than the exocyclic double bond, based on proxy alkenes (see Sect. 5). To our knowledge,
separate rate constants for NO$_3$ with the two double bonds in limonene have not been measured.

The absolute organic nitrate yield of the NO$_3$+limonene reaction can be estimated from instantaneous changes in $\Sigma$RONO$_2$ signal coincident with titration of limonene. The apparent nitrate yield during limonene consumption ($\Delta \Sigma$RONO$_2$/\Delta Limonene) is approximately 15% for both limonene injections, but this ignores the reaction of 50% of the limonene with O$_3$. Hence, the initial alkyl nitrate yield from NO$_3$+limonene reactions alone is approximately 30%.

The alkyl nitrate yield (including additional nitrate production after the complete consumption of limonene) is variable between the two injections. The net alkyl nitrate formed after the first and second injections of 10 ppb limonene were 1 and 3 ppb, corresponding to overall nitrate yields of 10% and 30%, respectively; however, as discussed below, the later formation of gaseous organic nitrate is complicated.

4.2 Aerosol mass yield

Aerosol formation was observed after each of two limonene injections. To determine aerosol yield, we first correct the aerosol mass loading for dilution and wall losses. We then calculate the mass yield as:

$$ Y = \frac{\Delta M}{\Delta VOC} $$

where $\Delta M$ is the corrected aerosol mass loading (µg m$^{-3}$) and $\Delta$VOC is the total reacted concentration (µg m$^{-3}$) of limonene. The yields are determined relative to each of the two separate injections of limonene, i.e., SOA formed from the first injection is simply considered “background” aerosol for the second injection. The final SOA yields observed (Fig. 2) at the peak aerosol concentration following each injection were 25% for the first injection and 40% after the second injection, suggesting that the presence in the second case of 10 µg m$^{-3}$ of existing aerosol from the first injection enhanced partitioning to the aerosol phase.
As seen in Eq. (1), these mass-based yields are calculated relative to limonene reacted. Hence, it is important in the interpretation of these yields to recall that oxidation of both double bonds in limonene adds significant additional mass to the molecule. If we assume the average molecular weight of aerosol-forming species is 250 g/mole, corresponding to limonene (C\textsubscript{10}H\textsubscript{16}) with addition of a nitrate group (NO\textsubscript{3}) and hydroxyl group (OH), the yield on a per-molecule basis would be 14–22%.

Following the first limonene injection, the relative SOA yields from two generations of oxidation (the oxidation of first the endo-, then the exocyclic double bonds in limonene) can be observed (Fig. 2), separated by their differing timescale. Oxidation of the first double bond in limonene by O\textsubscript{3} and NO\textsubscript{3} results in a 10% yield of SOA. The necessity for very low volatility nucleating species in this initial aerosol formation contributed to the low mass yield; while after the second injection, products of intermediate volatility could condense onto pre-existing aerosol.

Both limonene injections show relatively low initial gas-phase nitrate yields, measured as the increase in TD-LIF observed \(\Sigma RONO\textsubscript{2}\) divided by the decrease in limonene. This indicates that NO\textsubscript{3}-limonene reactions preferentially form the non-nitrate ketone product channels. Nevertheless, these reactions constitute an efficient pathway for SOA formation. On average, 15% of the aerosol mass is constituted of nitrate (NO\textsubscript{3}, MW=62).

5 Interpretation

5.1 Proposed reaction mechanism

Limonene is oxidized by both NO\textsubscript{3} and O\textsubscript{3}, as outlined in the mechanism shown in Fig. 3. The two double bonds in limonene allow the possibility of at least two NO\textsubscript{3} oxidation steps, each of which can produce an organic nitrate or non-nitrate; for simplicity we assume that the non-nitrate channel produces a ketone. This assumption is based on ketones being the highest yield non-nitrate product observed in reactions of NO\textsubscript{3} with
a variety of alkenes (Table III-D-1, Calvert et al., 2000). Either double bond can also react with \( \text{O}_3 \), the products of which have been determined in other chamber studies (Maksymiuk et al., 2009): the major O3LIM product is a C\textsubscript{10} backbone with a carbonyl and a carboxyl functional group added. As the limonene backbone becomes increasingly oxidized, these products can partition to the aerosol phase, generating SOA. We construct a mechanism and use observations to constrain the poorly known parameters, including the relative rates of \( \text{NO}_3 \) oxidation of the first and second double bond, the branching ratio of organic nitrate vs. ketone formation, and the gas-aerosol partitioning of the oxidation products.

### 5.1.1 Gas-phase kinetics

The full reaction scheme shown above (Fig. 3) is explicitly modeled with rate constants as tabulated in Table 2. Each double bond reacts with either \( \text{NO}_3 \) or \( \text{O}_3 \), at both first and second generations of oxidation.

In a base case model, we assume the non-specific rate constant measured for \( \text{NO}_3 + \text{limonene} \) was the rate for the faster reaction at the endocyclic double bond (\( 1.2 \times 10^{-11} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1} \) at 298 K, Calvert et al. (2000), chamber temperature ranged 294–296 K during the oxidation, so no temperature dependence was assumed). We apply the ratio of the measured rate constants for \( \text{NO}_3 \) with 2-methyl-propene (\( 3.1 \times 10^{-13} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1} \), proxy for the exocyclic double bond) to \( \text{NO}_3 \) with 2-methyl-2-butene (\( 9.3 \times 10^{-12} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1} \), proxy for the endocyclic double bond) to determine the rate of the slower reaction at the exocyclic double bond (\( 4.0 \times 10^{-13} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1} \)). The measured \( \text{O}_3 + \text{limonene} \) rate of \( 2.0 \times 10^{-16} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1} \) (Calvert et al., 2000) is assumed to be the total rate constant for both double bonds, with the reaction occurring 15% of the time at exocyclic double bond and 85% of the time at the endocyclic double bond, following Leungsakul et al. (2005). Applying instead the factor of 30 between rate constants at the two double bonds derived by another recent study (Donahue et al., 2007) does not significantly
affect results; essentially only the major product channel influences subsequent chem-
istry in either case. Reactions of O$_3$ or NO$_3$ with first-generation oxidation products of
limonene are assumed to proceed at the same rate as on limonene itself, i.e., oxidation
of one double bond does not affect rate constants at the other double bond. This is
in contrast to recent studies on isoprene nitrates (Lockwood et al., 2010), which found
that the nitrate group $\beta$ to the double bond increased its reaction rate with O$_3$. Since
in this case the double bonds are separated by three bonds, we assume the effect is
negligible.

The reaction of NO$_3$ with aldehydes produced in early generations of the chemistry
are also important. The rate constants used here are estimated based on a compre-
prehensive study of the kinetics of NO$_3$ reaction with a series of aldehydes (D’Anna et al.,
2001).

Wall loss rates of reactive species are determined from the timescale of NO$_3$, O$_3$,
and N$_2$O$_5$ loss in an earlier VOC-free chamber experiment, and aerosol loss rates
from observed particle number density decay during this experiment. Values for the
branching ratios for nitrate versus ketone production at each NO$_3$ oxidation step are
assumed to be independent of other functional groups on the molecule. The organic
nitrate branching ratios are estimated to be 32% at the exo double bond and 14% at
the endo double bond, based on overall nitrate branching ratios for $\alpha$- and $\beta$-pinene in
the Master Chemical Mechanism v3.1 (Saunders et al., 2003).

In this base case model, NO$_3$ and N$_2$O$_5$ are always underpredicted, while organic
nitrate is initially over predicted (after the first limonene addition, hours 4–7) and later
under-predicted (hours 9–24). The model/measurement discrepancy is improved by
systematically adjusting a number of the parameters in the gas phase mechanism,
subject to observational constraints, which are summarized in Table 1.

Since the concentrations of NO$_3$ and N$_2$O$_5$ are determined by their source (R1) and
sinks, and the source is well constrained, we adjust the modeled NO$_3$ sinks to find the
best agreement between modeled and measured NO$_3$ and N$_2$O$_5$ after limonene has
fully reacted after the first injection (hours 4–7, Fig. 4). The primary sinks of NO$_3$ are
reaction with limonene and its oxidation products. We find the best agreement using rate constants for NO$_3^-$ with limonene and its oxidation products that are a factor of two lower than the literature value (Calvert et al., 2000).

During the first limonene oxidation event, consumption of limonene by O$_3$ was appreciable relative to NO$_3^-$ oxidation (approximately 25% of the limonene is consumed by ozone), since the O$_3$ was injected after limonene and therefore the NO$_3^-$+limonene reaction was limited by the NO$_3^-$ production rate. We observe organic nitrate products to appear immediately in both gas and aerosol phase.

Finally, we tune the unknown rate constant of the larger aldehydes formed in the oxidation mechanism, TRIKET, G2O3 and DIKETONO3, with NO$_3^-$ using the total HNO$_3$ produced in the experiment (≈2 ppb) as a constraint, since these are the sole sources of nitric acid. We find the rate of NO$_3^-$+TRIKET or DIKETONO3 to be 50 times the rate of NO$_3^-$+HCHO, a reasonable range for a larger aldehyde (D’Anna et al., 2001).

These three constraints result in gas-phase chemistry that reproduces the concentrations after the first limonene injection reasonably well (Fig. 4). However, we note that the model overestimates NO$_3^-$ and that the second pulse of aerosol nitrate is overpredicted by about 30% before the second limonene injection (at hour 9).

5.1.2 Modeling aerosol partitioning of condensing species

We model the gas-aerosol partitioning of the limonene oxidation products using the equilibrium absorptive partitioning formalism, following Pankow and Capouet (Pankow, 1994; Capouet and Muller, 2006):

$$K_p = \frac{F/TSP}{A} = \frac{760 \cdot R \cdot T \cdot f_{om}}{MW_{om} \cdot 10^6 \cdot \zeta \cdot \rho_{vap}}$$

(F and A are the total aerosol-phase and gaseous concentrations of the compound of interest, and TSP is the concentration of total suspended particulate matter. In the second expression showing the equilibrium constant in terms of thermodynamic properties, R is the universal gas constant.)
(8.314 J mol\(^{-1}\) K\(^{-1}\) = 8.206 × 10\(^{-5}\) atm m\(^3\) K\(^{-1}\) mol\(^{-1}\)), \(T\) is temperature (K), \(f_{om}\) is the weight fraction of organic matter in the total aerosol (=1 for these experiments), \(MW_{om}\) is the average molecular weight of the absorbing organic material (g mol\(^{-1}\)), \(\zeta\) is the activity coefficient of the compound of interest in the condensed phase (assumed = 1 for these experiments), and \(p_{vap}\) is the subcooled vapor pressure of the compound of interest (Torr); 760 (Torr atm\(^{-1}\)) and 10\(^6\) (µg g\(^{-1}\)) are conversion factors. This gives \(K_p\) in units of m\(^3\) µg\(^{-1}\).

We explicitly model the equilibrium gas/aerosol partitioning of 11 condensable species: EXONO3/ENDONO3 (same \(p_{vap}\)), DINO3, KETONO3/O3LIM2NO3 (same \(p_{vap}\)), DIKETONO3/O3LIMNO3 (same \(p_{vap}\)), TRIKET, G2O3, and O3LIM/O3LIM2 (same \(p_{vap}\) assumed for \(O_3\) product from either double bond). For each, we calculate \(p_{vap}\) based on the proposed product structures shown in Fig. 3 and the group contribution method of Pankow and Asher (2008). These calculated values and the tuned values used in the present model are reported in Table 3. To initiate aerosol formation, a small amount of “seed” aerosol is injected in the model at the moment of ozone injection into the limonene; the seed does not affect ultimate aerosol yield in this equilibrium model. Partitioning is implemented by determining the gas-phase and aerosol fractions of each species at each time step, assuming that this partitioning is effectively instantaneous.

As has been noted in previous studies (Leungsakul et al., 2005; Fry et al., 2009), the predicted vapor pressures underestimates the aerosol produced. This suggests that the actual structures of limonene oxidation products are either more oxidized or oligomerized forms of the proposed structures, or that the group contribution method overestimates vapor pressure.

We employ the observed mass loading of organic and nitrate aerosol from the AMS as well as the observed gas/aerosol partitioning of organic nitrate after the first limonene injection as constraints to determine tuning factors to apply to the \(p_{vap}\)’s in the model. The shape of the time trace allows distinction between first- and
second-generation oxidation products. Measurement/model agreement on the organic and nitrate aerosol loading before and after tuning vapor pressures are shown in Fig. 5. After determining the tuning factors that best approximate the experimental data, the same group contribution method can be used to rationalize those factors applied. Most striking is the need for both first- and second-generation NO$_3$ products to have significantly lower volatility. For example, the shift in DIKETONO3’s vapor pressure could be caused by adding two carbonyl groups to the backbone. Two carbonyls lower the vapor pressure roughly half as much as one hydroxyl group. This high degree of oxidation is consistent with recent work on the ozone/limonene system (Bateman et al., 2009).

Initially, only one-fifth the observed aerosol nitrate after the first limonene injection was produced in the model. The vapor pressures were fit to the first nine hours of observed gas and aerosol phase nitrates, greatly improving measurement/model agreement (Fig. 4). This is a function both of the reduced vapor pressures of the nitrates themselves, and of having in general more organic aerosol mass onto which organic nitrates can partition.

5.2 Interpreting nitrate and aerosol formation after second limonene injection

Kinetic modeling captures limonene consumption by NO$_3$ and O$_3$, initial alkyl nitrate yields, overall aerosol yield and organic to nitrate ratio of the aerosol produced. However, the agreement between model and experimental observations of NO$_3$ shown in Fig. 4 does not persist through the second limonene injection. Without further changes, the gas-phase organic nitrate from hour 10 onwards is drastically underpredicted, while NO$_3$ is overpredicted. Because the maximum discrepancy coincides with the highest aerosol loading, reaction of NO$_3$ on the surface of the organic aerosol to produce an RONO$_2$ species that is more volatile than its parent aerosol-bound VOC is suggested. We model the aerosol uptake of NO$_3$ using:

\[
k_{\text{uptake}} = \gamma \frac{\nu_{\text{NO}_3} \cdot \text{SA}}{4}
\]
where $\gamma$ is the unitless uptake coefficient, $v_{NO_3}$ is the molecular speed of NO$_3$ (cm s$^{-1}$), and SA is the total aerosol surface area per volume (cm$^2$ cm$^{-3}$) calculated from the modeled aerosol mass, assumed density (1.6 g cm$^{-3}$, Fry et al., 2009) and measured mode particle radius (AMS). For the purposes of this modeling, we assume the limiting case: that every organic nitrate produced by this reaction evaporates to the gas phase. We multiply SA by the (modeled) fraction of aerosol containing unsaturated double bonds to more easily enable comparison to uptake measurements on well-defined hydrocarbon surfaces. With the observed and modeled aerosol surface area peaking at $1.3 \times 10^{-6}$ cm$^2$ cm$^{-3}$, an uptake coefficient of NO$_3$ onto the fraction of the aerosol that contains double bonds of $\gamma \approx 5 \times 10^{-1}$ provides the best fit to the gas/aerosol nitrate partitioning after the 2nd limonene injection (Fig. 6). This uptake coefficient was determined using observed NO$_3$; the figure shows the resulting improvement of fit in the full model using this $\gamma$. In this experiment, the double-bond containing fraction of the aerosol ranges between 10% and 40%, meaning the uptake coefficient on the total aerosol formed in the SAPHIR chamber ranged between $\gamma = 0.05 - 0.2$.

This value of uptake coefficient is in general agreement with the results of Gross and Bertram (2009), who measured uptake coefficients around $2 \times 10^{-3}$ on neat liquid surfaces of saturated ethers and polyols, up to $2 \times 10^{-1}$ for a mono-unsaturated carboxylic acid. Under the dry conditions of the present experiment, heterogeneous uptake of N$_2$O$_5$ was expected to be negligible. In our previous study on SOA formation from NO$_3$+$\beta$-pinene (Fry et al., 2009), we found that we did not need to include any heterogeneous chemistry to explain observations. This is reasonable, since in that study the aerosol formed by NO$_3$ reaction with the monounsaturated alkene would not have contained double bonds. Given the low aerosol surface area in that study and using the measured uptake coefficient for NO$_3$ on saturated alkanes of around $10^{-3}$ (Gross and Bertram, 2009; Moise et al., 2002), the heterogeneous loss rate of NO$_3$ was negligibly small. In contrast, in this limonene experiment the aerosol contains some unsaturated double bonds, leading to a higher uptake coefficient and significant heterogeneous NO$_3$ uptake.
Given the underpredicted aerosol formation from our raw reaction mechanism, this model is almost certainly incomplete in terms of later oxidation steps. Therefore, it is possible that a late-peaking gas-phase species is instead responsible for this very efficient observed conversion of NO$_3$ to volatile organic nitrate; however, as will be shown below, there is additional evidence in the AMS data for consumption of organic aerosol that bolsters this hypothesis of heterogeneous NO$_3$ reactions.

Despite the improvement in modeling gas/aerosol partitioning of organic nitrate with this heterogeneous process included, no reasonable permutations on the rate constants or partitioning constants of mechanism described thus far can fully reproduce the major unique feature of this “second experiment”: the pronounced dip in NO$_3$ and N$_2$O$_5$ around 12 h. Figure 7 shows the measured and modeled NO$_3$ and N$_2$O$_5$ with the complete model described here. A slight dip appears due to the heterogeneous uptake of NO$_3$, but not nearly as abrupt nor with as dramatic a recovery as observed in the data. We have attempted increasing the rate of that process, as well as all other NO$_3$ sinks in the present mechanism. In all cases, this further depletes NO$_3$/N$_2$O$_5$ everywhere rather than simply deepening the dip. What appears to be necessary is a chemical process that is activated only at hour 11 and ceases at hour 13. This remains a major gap in the modeling of this system, which we have not been able to resolve with the mechanism described here.

Table 1 summarizes all tuned parameters in the gas and aerosol model and the observations used to constrain each.

### 5.3 Aerosol chemical composition

As in previous investigations of the SOA formation from reactions of NO$_3$ with biogenic VOCs (β-pinene, Fry et al. (2009) and isoprene, Rollins et al. (2009)), the main characteristic feature of the organic nitrates is a low NO$_3^+$/NO$_2^+$ ratio. In addition, the m/z 76 (CH$_2$NO$_3^+$) ion fragment again appears as an indicator for the presence of organic nitrates. Beyond this, the AMS observations diverge from previous experiments somewhat. Here, a heavier m/z 184 (C$_9$H$_{14}$NO$_3^+$) fragment is clearly present throughout
the experiment (Fig. 8). The increase in this fragment over the course of the experiment suggests that larger nitrates are incorporated into the aerosol via later-generation chemistry.

In order to further assess SOA chemistry (ozonolysis versus NO$_3$ oxidation sources, first versus second generation oxidation), the AMS organic aerosol fraction was analyzed using positive matrix factorization (PMF) (Paatero and Tapper, 1994; Paatero, 1997). This analysis was performed entirely independent of the above described kinetics modeling. The PMF analysis applied principles and utilized code as introduced by Ulbrich et al. (2009). The number of factors used to describe the total aerosol formed was selected based on the residuals both in MS and time space. Since the sources for aerosol formation were reactions of limonene with NO$_3$ and O$_3$, the nitrate that was observed in the course of the experiment was included in the PMF analysis. Three factors were found to describe the measured data with residuals below 2% at all times (Fig. 9).

The resolved PMF components (Fig. 10) can be interpreted based upon the correlation of their time derivatives with rates of selected processes based on modeled species. Factor 1 has high nitrate content ($m/z$ 30 and 46 contribute 12% to the factor 1 mass), and the ratio of 46/30 is 0.13, well below the typical ratio observed for NH$_4$NO$_3$. It is also correlated to the AMS measured nitrate ($R^2$=0.95) and is thus interpreted as organic nitrate. Of the modeled organic nitrate production rates, factor 1 correlates poorly with first-generation production ([NO3]×[LIM], $R^2$=0.46), but correlates well with second-generation production from ozone oxidation of first generation nitrates ([O3]×[ENDONO3], $R^2$=0.83). It is not at all correlated with NO$_3$ oxidation of first-generation ozone products.

The second factor is better correlated with first-generation ozone oxidation of limonene ([O3]×[LIM], $R^2$=0.73) than second-generation ([O3]×[O3LIM], $R^2$=0.26). Its mass spectral pattern supports the interpretation of oxidized organics from the first generation reaction of O$_3$ with limonene.
The third component also contains significant organic nitrate: the ratio of 46/30 is 0.17 for factor 3 and the sum of 30 and 46 contribute 19% of the total mass of this factor. It is best correlated with reaction of NO₃ with ozone-produced aerosol ([NO₃]×[O₃LIMaero], $R^2=0.73$). A correlation almost as good is found using [NO₃]×SA, weighted by factor 2 ($R^2=0.61$), which was attributed to the purely ozone-generated aerosol. We therefore interpret factor 3 as representing heterogeneous uptake processes on the SOA in the second part of the experiment. The decay of the organic factor 2 coincident with increase in this factor also supports this interpretation. It is possible that NO₃ uptake onto limonene SOA results sometimes in revolatilization of an organic nitrate (as invoked in this model), sometimes in net uptake of nitrate, creating larger multifunctional nitrates which remain in the aerosol phase, and sometimes in NO₂ release and chemical conversion of the aerosol phase.

6 Conclusions

Observations of the reaction of NO₃ with limonene show that the RONO₂ yield is approximately 30%, implying significant release of the nitrate functional group after attack at the double bonds. The aerosol mass yield is 25–40%. We find that aerosol composition is affected by NO₃ reaction with increased incorporation of organic nitrate into the aerosol over time and apparent conversion of aerosol bound alkene moieties to nitrate moieties. These conclusions bolster other recent evidence suggesting that nitrate addition to monoterpenes may be an important player in the aerosol budget in those locations where biogenic terpene emissions are large and NOₓ is abundant.

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Secondary organic aerosol from NO$_3$+limonene

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Table 1. Parameters that were tuned in this model to best fit the observational data, along with the observational constraints used to determine best fit.

<table>
<thead>
<tr>
<th>Tuned parameter</th>
<th>Observational constraint</th>
<th>Value used in model</th>
</tr>
</thead>
<tbody>
<tr>
<td>Rate of NO$_3$+LIM</td>
<td>Limonene decay; total NO$_3$+N$_2$O$_5$, hours 4–7</td>
<td>6.0×10$^{-12}$, Calvert et al., 2000 (÷2)</td>
</tr>
<tr>
<td>Rate of NO$_3$+O3LIM</td>
<td>Alkyl nitrate formation after 1st injection</td>
<td>0</td>
</tr>
<tr>
<td>Ratio of rates of NO$_3$+endo vs. exo C=C</td>
<td>Overall NO$_3$/N$_2$O$_5$ shape after 1st injection</td>
<td>30</td>
</tr>
<tr>
<td>Rate of NO$_3$+later-gen. aldehydes</td>
<td>HNO$_3$ production</td>
<td>50×NO$_3$+HCHO rate</td>
</tr>
<tr>
<td>Tuning factors for all $p_{vap}$</td>
<td>Gas/aerosol partitioning of nitrate after 1st injection; organic / nitrate aerosol loading</td>
<td>See Table 3</td>
</tr>
<tr>
<td>$\gamma_{NO_3\text{-aerosol}}$</td>
<td>Gas/aerosol partitioning of nitrate after 2nd injection</td>
<td>0.2</td>
</tr>
</tbody>
</table>
Table 2. Reaction rate constants and branching ratios used in gas-phase portion of kinetics box model. For structures corresponding to variable names, see reaction scheme figure.

<table>
<thead>
<tr>
<th>Reaction</th>
<th>Branching ratio</th>
<th>Rate constant (cm$^3$ molec$^{-1}$ s$^{-1}$, 298 K unless otherwise indicated)</th>
<th>Reference/Notes</th>
</tr>
</thead>
<tbody>
<tr>
<td>NO$_3$+O$_2$→NO$_3$</td>
<td></td>
<td></td>
<td>JPL Kinetics Eval 15, July 2007</td>
</tr>
<tr>
<td>NO$_3$+NO$_2$→N$_2$O$_5$</td>
<td></td>
<td></td>
<td>JPL Kinetics Eval 15, July 2007</td>
</tr>
<tr>
<td>N$_2$O$_5$→NO$_3$+NO$_2$</td>
<td></td>
<td>2.13×10$^{-27}$×exp(11025/T)</td>
<td>Based on equilibrium constant measured at Juelich, July 2007</td>
</tr>
</tbody>
</table>

| NO$_3$+LIM→ENDONO3 | 0.14 | 6.0×10$^{-12}$ | Calvert et al., 2000 (+2) |
| NO$_3$+LIM→ENDOLIM+NO$_2$ | 0.86 | 6.0×10$^{-12}$ | ibid. |
| NO$_3$+LIM→EXONO3 | 0.32 | 2.0×10$^{-13}$ | Above +30, see text |
| NO$_3$+LIMONE→HCHO | 0.68 | 2.0×10$^{-13}$ | ibid. |
| NO$_3$+EXONO3→DINO3 | 0.14 | 6.0×10$^{-12}$ | Same as rate at endo bond in bare limonene |
| NO$_3$+EXONO3→DIKETONO3 | 0.86 | 6.0×10$^{-12}$ | ibid. |
| NO$_3$+LIMONE→KETONO3 | 0.14 | 6.0×10$^{-12}$ | ibid. |
| NO$_3$+LIMONE→TRIKET | 0.86 | 6.0×10$^{-12}$ | ibid. |
| NO$_3$+ENDONO3→DINO3 | 0.32 | 2.0×10$^{-13}$ | Same as rate at exo bond in bare limonene |
| NO$_3$+ENDONO3→KETONO3+HCHO+NO$_2$ | 0.68 | 2.0×10$^{-13}$ | ibid. |
| NO$_3$+ENDOLIM→DIKETONO3 | 0.32 | 2.0×10$^{-13}$ | ibid. |
| NO$_3$+ENDOLIM→TRIKET | 0.68 | 2.0×10$^{-13}$ | ibid. |
| NO$_3$+TRIKET→G3KET+HNO$_3$ | 5.0×10$^{-14}$ | 50×rate of NO$_3$+HCHO; see text |
| NO$_3$+G2O3→G3O3+HNO$_3$ | 5.0×10$^{-14}$ | ibid. |
| NO$_3$+DIKETONO3→G3NO3+ | 5.0×10$^{-14}$ | ibid. |
| O$_3$+LIM→O3LIM (endo) | 1.7×10$^{-16}$ | 85% of total O$_3$+LIM, Calvert et al., 2000 |
| O$_3$+LIM→O3LIM2 (exo) | 3.0×10$^{-17}$ | 15% of total O$_3$+LIM, Calvert et al., 2000 |
| O$_3$+O3LIM→G2O3+TRIKET | 3.0×10$^{-17}$ | Same as rate at exo bond in bare limonene |
| O$_3$+O3LIM→G2O3+TRIKET | 1.7×10$^{-16}$ | Same as rate at endo bond in bare limonene |
| NO$_3$+O3LIM→O3LIMNO3 | <4.0×10$^{-16}$ | Rate of NO$_3$+LIM (exo)+50 is upper limit; see text |
| NO$_3$+O3LIM→O3LIM2NO3=KETONO3 | <1.2×10$^{-13}$ | Rate of NO$_3$+LIM (endo)+50 is upper limit; see text |
| O$_3$+ENDONO3→O3LIM2NO3=KETONO3 | 3.0×10$^{-17}$ | Same as rate at exo bond in bare limonene |
| O$_3$+ENDOLIM→G2O3=TRIKET | 3.0×10$^{-17}$ | Same as rate at exo bond in bare limonene |
| O$_3$+EXONO3→O3LIMNO3=DIKETONO3 | 1.7×10$^{-16}$ | Same as rate at endo bond in bare limonene |
| O$_3$+LIMONE→G2O3=TRIKET | 1.7×10$^{-16}$ | Same as rate at endo bond in bare limonene |
| NO$_3$+walls→ | 6.0×10$^{-4}$ | from NO$_3$ loss timescale in VOC-free chamber |
| N$_2$O$_5$+walls→ | 7.2×10$^{-5}$ | from N$_2$O$_5$ loss timescale in VOC-free chamber |
| O$_3$+walls→ | 3.9×10$^{-6}$ | from O$_3$ loss timescale in VOC-free chamber |
| limonene oxidation products+walls→ | 1.8×10$^{-5}$ | fit to later alkyl nitrate decay |
Table 3. Parameters used in gas-aerosol partitioning portion of the kinetics box model. Calculated vapor pressures were determined using the formalism of Pankow and Asher (2008). For reference, the $p_{vap}$ determined for a pinene monohydroxynitrate was $4.0 \times 10^{-5}$ Torr (Fry et al., 2009).

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Calculated value (Torr)</th>
<th>Adjusted value (Torr)</th>
<th>Approx. equivalent structural change</th>
</tr>
</thead>
<tbody>
<tr>
<td>$p_{vap}$ (EXONO3 and ENDONO3)</td>
<td>$2.9 \times 10^{-5}$</td>
<td>$5.8 \times 10^{-7}$</td>
<td>Add 2 ketones</td>
</tr>
<tr>
<td>$p_{vap}$ (DINO3)</td>
<td>$8.2 \times 10^{-10}$</td>
<td>$8.2 \times 10^{-11}$</td>
<td>Add 1 ketone</td>
</tr>
<tr>
<td>$p_{vap}$ (KETONO3)</td>
<td>$9.6 \times 10^{-6}$</td>
<td>$9.6 \times 10^{-7}$</td>
<td>Add 1 ketone</td>
</tr>
<tr>
<td>$p_{vap}$ (DIKETONO3 and O3LIMNO3)</td>
<td>$5.0 \times 10^{-7}$</td>
<td>$5.0 \times 10^{-9}$</td>
<td>Add 2 ketones</td>
</tr>
<tr>
<td>$p_{vap}$ (TRIKET)</td>
<td>$5.8 \times 10^{-3}$</td>
<td>$5.8 \times 10^{-3}$</td>
<td>No change</td>
</tr>
<tr>
<td>$p_{vap}$ (O3LIM)</td>
<td>$7.4 \times 10^{-5}$</td>
<td>$7.4 \times 10^{-6}$</td>
<td>Add 1 ketone</td>
</tr>
<tr>
<td>$p_{vap}$ (G2O3)</td>
<td>$3.1 \times 10^{-5}$</td>
<td>$3.1 \times 10^{-6}$</td>
<td>Add 1 ketone</td>
</tr>
</tbody>
</table>
Fig. 1. Overview time series of species monitored. Ethane was used as an inert dilution tracer. Chamber temperature was between 288–296 K for the duration of this experiment.
Fig. 2. Total limonene reacted and time-dependent, loss-corrected total aerosol yield for the two limonene injections. Increase in yield after limonene is depleted indicates that reaction at the second double bond in first-generation oxidation products produces aerosol.
Fig. 3. Reaction scheme of NO$_3$ and O$_3$ oxidation of limonene. Structures (especially O$_3$ products) are proposed approximations; names correspond to individual molecular species tracked in model mechanism.
Fig. 4. Measured (markers) and modeled (lines) time traces after the first limonene injection. Bottom panel shows the major products modeled.
Fig. 5. Change in measurement/model agreement of AMS-measured aerosol organic and aerosol nitrate mass loading before (dashed lines) and after (solid) tuning predicted vapor pressures.
Fig. 6. Change in measurement/model agreement of aerosol and total nitrate without (dashed lines) and with (solid) inclusion in the model of NO$_3$ uptake and revolatilization of organic nitrate. An uptake coefficient of $\gamma=0.5$ onto the double-bond containing fraction of aerosol gives the best agreement, equivalent to an overall uptake coefficient on this aerosol of $\gamma=0.05-0.2$. While the addition of this uptake process does not appreciably change the modeled nitrate aerosol, it does drops peak organic aerosol concentrations by about 5 $\mu$g m$^{-3}$, from 26 to 21 $\mu$g m$^{-3}$. The optimized model traces in Fig. 5 include this uptake process.
Fig. 7. Measurement/model agreement of NO$_3$ and N$_2$O$_5$ after the second limonene injection. No reasonable permutations of model parameters achieved better agreement with the NO$_3$ “dip”.
Fig. 8. AMS-detected organo-nitrates fragments. For reference, $\text{C}_6\text{H}_4^+$ is also shown, a fragment which occurs at the same nominal $m/z$ as $\text{CH}_2\text{NO}_3^+$. 
Fig. 9. Summary of PMF results. Upper panel: measured mass in each factor (1: black, 2: red, and 3: green). After these three mass factors, residuals were below ±2% for the entire experiment. Lower panels: correlation plots of the time derivative of each factor with the rate of the best correlated chemical process.
Fig. 10. Mass spectra of the three factors derived from PMF analysis with inserts showing expanded views. Factor one (black) is characterized by a large contribution from m/z 43 and significant 30 and 46. Factor two (red) has a significant signal on m/z 44 and 39, suggesting oxidized organics, and has no contribution from the nitrate masses. Factor three (green) has the largest relative contribution from nitrate masses and larger contributions on m/z >100 than factor 1.