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Estimating collision efficiencies from contact freezing experiments

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Abstract

Interactions of atmospheric aerosols with clouds influence cloud properties and modify the aerosol life cycle. Aerosol particles act as cloud condensation nuclei and ice nucleating particles or become incorporated into cloud droplets by scavenging. For an accurate description of aerosol scavenging and ice nucleation in contact mode, collision efficiency between droplets and aerosol particles needs to be known. This study derives the collision rate from experimental contact freezing data obtained with the ETH Collision Ice Nucleation Chamber CLINCH. Freely falling 80 μm water droplets are exposed to an aerosol consisting of 200 nm diameter silver iodide particles of concentrations from 500–5000 cm^{-3} , which act as ice nucleating particles in contact mode. The chamber is kept at ice saturation in the temperature range from 236–261 K leading to slow evaporation of water droplets giving rise to thermophoresis and diffusio-phoresis. Droplets and particles bear charges inducing electrophoresis. The experimentally derived collision efficiency of 0.13 is around one order of magnitude higher than theoretical formulations which include Brownian diffusion, impaction, interception, thermophoretic, diffusio-phoretic and electric forces. This discrepancy is most probably due to uncertainties and inaccuracies in the description of thermophoretic and diffusio-phoretic processes acting together. This is to the authors knowledge the first dataset of collision efficiencies acquired below 273 K. More such experiments with different droplet and particle diameters are needed to improve our understanding of collision processes acting together.

1 Introduction

Interactions of atmospheric aerosols with clouds influence the cloud properties and modify the aerosol life cycle. Depending on particle size, morphology and chemical composition, aerosol particles act as cloud condensation nuclei (CCN) and ice nucleating particles (INP) or become incorporated into cloud droplets by scavenging. Scav-

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cesses. Accurate estimates of collision efficiencies are also needed to describe cloud glaciation. Up to date, there is lack of atmospheric INP that might explain ice nucleation at temperatures higher than -15°C . While biological particles are discussed as candidates to close this gap (DeMott et al., 2010), an alternative explanation would be ice nucleation in contact mode. Several field studies have observed that ice crystals preferentially formed in regions of downdrafts and at cloud edges where dry air is entrained (Young, 1974). Particles contained in these air masses could initiate droplet freezing when they collide with them. To judge the importance of this process nucleation and collision efficiencies have to be quantified. The representation of heterogeneous ice nucleation in most global models still lacks a detailed description of the freezing processes depending on aerosol properties and nucleation mode (Yun and Penner, 2012; Lohmann and Hoose, 2009).

Depending on particle size and the forces acting on the particles, different collision processes have to be taken into account. In models, collision efficiencies are usually calculated as the sum of the different collision processes (Andronache et al., 2006; Bae et al., 2009; Croft et al., 2010) neglecting that the forces act together to determine the aerosol path either into or around the droplet. Trajectory calculations can be used to simulate the particle pathway, however, they need to be validated with reliable laboratory measurements (Tinsley and Leddon, 2013). Calculated collision efficiencies are quite accurate for Aitken and coarse mode particles, for which either Brownian diffusion or impaction dominates. Accumulation mode particles fall into the particle size range of the Greenfield gap (Greenfield, 1957; Seinfeld and Pandis, 2006; Ladino et al., 2011a), where Brownian diffusion and impaction are inefficient collision mechanisms. However, the collision efficiency minimum of the Greenfield gap is reduced in the presence of electric or phoretic forces and theoretical descriptions have to include the corresponding contributions to the collision efficiencies to give accurate values. Only few experimental studies have explored this part of the parameter space (Ladino et al., 2011a; Ladino, 2011) and none of them at mixed-phase cloud temperatures.

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path and lead to the collision of aerosols with droplets (Ladino et al., 2011b). For the smallest particles, Brownian diffusion is the most important collision process. Brownian diffusion describes the random motion of aerosol particles resulting from collisions with carrier gas molecules. It is a strong function of particle size being most important for small aerosol particles. Large particles are most efficiently scavenged by inertial interception and impaction. Inertial impaction occurs when a particle is unable to follow the streamlines around a falling droplet and, because of its inertia, continues to move toward the drop and is eventually captured by it (Seinfeld and Pandis, 2006). Interception takes place when a particle follows the streamlines around a falling droplet sufficiently close to collide with it. The region of low collision efficiency between the small and large aerosol particles is known as the Greenfield gap. This gap may at least be partly closed when electric and phoretic effects contribute to particle collisions. Thermophoresis describes a net transport of particles in the presence of a temperature gradient in the air. Air molecules at higher temperature have a higher mean velocity and therefore impart more momentum on a particle than colder ones. The momentum on the warmer side of the particle is therefore larger and moves particles from higher to lower temperatures. Since evaporation cools the droplets and induces a temperature gradient in the surrounding air, particles are attracted by droplets for $RH < 100\%$ because of thermophoresis. Diffusiophoresis arises in the presence of a vapor concentration gradient. In the case of an evaporating droplet, there is a flux of water molecules away from the droplet, compensated by a flux of carrier gas molecules (mainly N_2 , O_2) in the opposite direction (Stephan flow) to keep the total pressure constant. These flows exert a repulsive force on the particle. Under typical atmospheric conditions thermophoresis dominates diffusiophoresis for aerosol particles $< 1\ \mu\text{m}$ (Slinn and Hales, 1971). Finally, in case of charged particles and droplets, electroscavenging has to be considered as an additional collision process. Usually, collision efficiencies of each of these processes are formulated separately and added together to yield the total collision efficiency E_{tot} . Park et al. (2005) and Slinn (1983) proposed formulations for the collision efficiencies by Brownian diffusion (E_{Br}), interception (E_{int}), and impaction (E_{imp}). Andronache

et al. (2006) gives formulations for thermophoresis (E_{Th}), diffusiophoresis (E_{Df}), and electrophoresis (E_{EI}). Wang et al. (1978) use a flux model to calculate collision rate coefficients for electric and phoretic scavenging. In the following, we will outline the formulations proposed for the different collision processes.

5 2.2 Brownian diffusion, interception and impaction

In the approaches by Park et al. (2005), hereafter referred to as P05, and Slinn (1983), hereafter referred to as S83, collision efficiencies of Brownian diffusion, interception and impaction ($E_{Br,l}$) are provided. They are calculated separately and added together.

$$E_{Br,l} = E_{Br} + E_{int} + E_{imp} \quad (1)$$

10 2.2.1 Formulation by Park (P05)

For collision efficiencies due to Brownian diffusion and interception Park et al. (2005) follow Jung and Lee (1998) who used a resolved flow field around a system consisting of multiple spheres to obtain an analytical solution including the effects of induced internal circulation inside a liquid droplet. Due to the influence of the internal flow, the outer flow velocity around the fluid spheres becomes larger than that around solid spheres. For this reason, the streamlines pass around a fluid sphere more closely than around a solid sphere. The collision efficiency due to Brownian diffusion is taken from Park et al. (2005):

$$E_{Br}(d_p, D_d) = 2 \left(\frac{\sqrt{3}\pi}{4P_e} \right)^{\frac{2}{3}} \left(\frac{(1-\alpha)(3\sigma+4)}{(J+\sigma K)} \right)^{\frac{1}{3}} \quad (2)$$

where α is the packing density i.e. the water volume present in a unit volume of air and σ the viscosity ratio of water to air. The hydrodynamic factors J and K are given as

$$J = 1 - \frac{6}{5}\alpha^{\frac{1}{3}} + \frac{1}{5}\alpha^2$$

$$K = 1 - \frac{9}{5}\alpha^{\frac{1}{3}} + \alpha + \frac{1}{5}\alpha^2$$

5 and P_e is the Peclet number defined as the ratio between the advective and diffusive transport rate and is given as

$$P_e = \frac{D_d U(D_d)}{D_{\text{diff}}}$$

where D_d is the droplet diameter, $U(D_d)$ is the terminal velocity of the drop and D_{diff} the diffusion coefficient of aerosol particles given by

$$10 \quad D_{\text{diff}} = \frac{k_B T_a C_c(d_p)}{3\pi\mu_a d_p}$$

where k_B is the Boltzmann constant, T_a is the air temperature in K, μ_a is the dynamic viscosity of air and $C_c(d_p)$ is the Cunningham slip correction factor to account for non-continuum effects associated with small particles. It is given as (Ladino et al., 2011a)

$$C_c(d_p) = 1 + \frac{2\lambda_a}{d_p} \left[1.257 + 0.4 \exp\left(\frac{-1.1d_p}{2\lambda_a}\right) \right]$$

15 where λ_a is the mean free path of air molecules. The temperature dependent viscosity of air μ_a is taken from the parametrization in Pruppacher and Klett (1997). In poise units it is given as

$$\mu_a = \frac{1.718 + 0.0049T_c - 0.000012T_c^2}{10^{-4}}$$

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where T_c is the temperature in °C. For the viscosity of water the lowest measured value at 273 K is used ($1.787 \times 10^{-3} \text{ kg m}^{-1} \text{ s}^{-1}$).

According to Jung and Lee (1998) the collision efficiency due to interception E_{int} is given as

$$E_{\text{int}}(d_p, D_d) = \frac{1 - \alpha}{J + \sigma K} \left[\frac{R}{1 + R} + \frac{1}{2} \left(\frac{R}{1 + R} \right)^2 (3\sigma + 4) \right] \quad (3)$$

where R is the diameter ratio between particle and droplet $\frac{d_p}{D_d}$.

The collision efficiency due to impaction E_{imp} is given as

$$E_{\text{imp}}(d_p, D_d) = \left(\frac{Stk}{Stk + 0.35} \right)^2 \quad (4)$$

where Stk is the Stokes number

$$Stk = \frac{\rho_p d_p^2 U(D_d)}{18 \mu_a D_d}$$

and ρ_p is the density of the particles.

2.2.2 Formulation by Slinn (S83)

Slinn (1983) proposed formulations for E_{Br} , E_{int} and E_{imp} using dimensional analysis coupled with experimental data which are summarized in Seinfeld and Pandis (2006).

Based on Slinn (1983), the following formulations are given in Seinfeld and Pandis

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(2006) and Wang et al. (2010)

$$E_{Br}(d_p, D_d) = \frac{4}{ReSc} (1 + 0.4Re^{\frac{1}{2}} Sc^{\frac{1}{3}} + 0.16Re^{\frac{1}{2}} Sc^{\frac{1}{2}}) \quad (5)$$

$$E_{int}(d_p, D_d) = 4 \frac{d_p}{D_d} \left[\frac{\mu_a}{\mu_w} + (1 + 2Re^{\frac{1}{2}}) \frac{d_p}{D_d} \right] \quad (6)$$

$$E_{imp}(d_p, D_d) = \left(\frac{\rho_w}{\rho_p} \right)^{\frac{1}{2}} \left(\frac{St - St^*}{St - St^* + \frac{2}{3}} \right)^{\frac{3}{2}} \quad (7)$$

5 where ρ_w and ρ_p are densities of liquid water and particles respectively. The normalizing factor $\frac{\rho_w}{\rho_p}$ is necessary to account for aerosol particles with density $> 1000 \text{ kg m}^{-3}$. Re is the Reynolds number representing the ratio of inertial to viscous forces in the flow and given by Pruppacher and Klett (1997).

$$Re = \exp(Y)$$

10 where Y is

$$Y = -3.18657 + 0.992696X - 0.00153193X^2 - 0.000987059X^3 \\ - 0.000578878X^4 + 0.000085517X^5 - 0.00000327815X^6$$

where $X = \ln(CdRe^2)$ and $CdRe^2$ is given as

$$CdRe^2 = \frac{4D_d^3(\rho_w - \rho_a)g}{3\mu_a^2}$$

15 where ρ_a is the density of air, g is the acceleration due to gravity. Sc is the Schmidt number of aerosol particles, St is the particle Stokes number given as

$$St = \frac{2\tau(U(D_d) - u(d_p))}{D_d}$$

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$U(D_d)$ and $u(d_p)$ are the terminal velocities of the droplets and aerosol particles, respectively. The relaxation time τ is given as (Wang et al., 2010),

$$\tau = \frac{(\rho_p - \rho_a)d_p^2 C_c}{18\mu_a}$$

St^* is the critical Stokes number above which particles may be deposited on the droplet. Note that S83 uses a slightly different formula for the Stokes number (St) than P05 (Stk). In the formulation for E_{imp} given in Eq. (7) collision can happen only when $St > St^*$. The critical Stokes number is given as

$$St^* = \frac{1.2 + \frac{1}{12} \ln(1 + Re)}{1 + \ln(1 + Re)}$$

2.3 Phoretic forces

Since inside the collision chamber, the droplets are evaporating, thermo- and diffusio-phoretic forces also contribute to the collision efficiency. Electroscavenging has to be taken into account because particles and droplets are charged. We consider the formulations of Andronache (2004); Andronache et al. (2006), hereafter referred to as A06, where collision efficiencies are calculated separately and added together to obtain the total collision efficiency due to phoretic forces E_{ph}

$$E_{ph} = E_{Th} + E_{Df} + E_{El} \quad (8)$$

where E_{Th} , E_{Df} and E_{El} are the collision efficiencies due to thermophoresis, diffusio-phoresis and electrophoresis, respectively.

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2.3.1 Formulation by Andronache (A06)

The contribution of thermophoresis to the collision efficiency is given as (Andronache et al., 2006)

$$E_{Th}(d_p, D_d) = \frac{4\gamma(2 + 0.6Re^{\frac{1}{2}}P_r^{\frac{1}{3}})(T_a - T_s)}{U(D_d)D_d} \quad (9)$$

- 5 where T_a is the absolute temperature of air, T_s is the absolute temperature at the droplet surface and P_r the Prandtl number for air given as

$$P_r = \frac{C_p \mu_a}{k_a}$$

γ is given as

$$\gamma = \frac{2C_c \left(k_a + 5 \frac{\lambda_a}{D_d} k_p \right) k_a}{5p \left(1 + 6 \frac{\lambda_a}{D_d} \right) \left(2k_a + k_p + 10 \frac{\lambda_a}{D_d} k_p \right)}$$

- 10 where k_a and k_p are the thermal conductivities of the air and the aerosol particles, p is the atmospheric pressure and C_p is the specific heat of air at constant pressure. The diffusiophoretic contribution to collision efficiency is given as

$$E_{Df}(d_p, D_d) = \frac{4\beta(2 + 0.6Re^{\frac{1}{2}}Sc_w^{\frac{1}{3}}) \left(\frac{\rho_s^0}{T_s} - \frac{\rho_a^0 RH}{T_a} \right)}{U(D_d)D_d} \quad (10)$$

where

$$15 \beta = \frac{T_a D_w}{p} \cdot \left(\frac{M_w}{M_a} \right)^{\frac{1}{2}}$$

The Schmidt number for water vapor in air is given as

$$Sc_w = \frac{\mu_a}{\rho_a D_w}$$

where D_w is the diffusivity of water vapor in air. For evaporating droplets, the diffusio-phoretic contribution to E is negative. In the formulation by Andronache et al. (2006), the contribution of electric charge to the scavenging efficiency is based on Coulomb interactions between aerosol particles and droplets carrying point charges of opposite sign, leading to the capture of particles present on the streamline close to the droplet surface. The expression for this electrostatic collision efficiency is given as (Andronache, 2004; Davenport and Peters, 1978)

$$E_{El}(d_p, D_d) = \frac{16KC_c Qq}{3\pi\mu_a D_d^2 d_p U(D_d)} \quad (11)$$

where $K = 9 \times 10^9 \text{ Nm}^2 \text{ C}^{-2}$, Q and q are the mean charges on the droplet and the aerosol particle in Coulomb units.

2.3.2 The flux model (W78)

An alternative formulation for phoretic and electrostatic forces is given by the flux model (Wang et al., 1978), hereafter referred to as W78. It expresses the thermophoretic force F_{Th} as (Tinsley et al., 2006)

$$F_{Th} = - \frac{6\pi\mu_a d_p (k_a + 2.5k_p Kn) k_a}{5(1 + 3Kn)(k_p + 2k_a + 5k_p Kn) \rho} \frac{2(T_a - T_s)}{D_d r^2} \quad (12)$$

where r is the distance between the center of the droplet and the particle and Kn the Knudsen number. The term $\frac{2(T_a - T_s)}{D_d r^2}$ is the temperature gradient between the absolute

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temperature of the surrounding (T_a) and at the droplet surface (T_s), assuming spherical symmetry. The diffusiophoretic force can be expressed as (Tinsley et al., 2006)

$$F_{Df} = -\frac{3\pi\mu_a d_p (0.74) D_w M_a 2(\rho_{v,a} - \rho_{v,s})}{(1 + \alpha Kn) M_w \rho_a D_d r^2} \quad (13)$$

The last term in this expression $\frac{2(\rho_{v,a} - \rho_{v,s})}{D_d r^2}$ is the gradient in water vapor density. M_a and M_w are the molecular weights of air and water, $\rho_{v,a}$ and $\rho_{v,s}$ are the water vapor densities in the air far from the droplet and at the droplet surface, respectively. The parameter α is given as (Wang et al., 1978)

$$\alpha = 1.26 + 0.40 \exp(-1.10 Kn^{-1})$$

The formulation of the forces is strictly valid only for spherically symmetric inverse square fields. This is the case for stationary droplets. If the droplet moves, the temperature and vapor fields are not spherically symmetric. As a first order correction, mean heat and vapor ventilation coefficients f_h and f_v , respectively, can be introduced to account for the effect of air motion on the flux of heat and water vapor (Tinsley, 2010). With this correction, the forces may be expressed as $F_{Th} = \frac{C_{Th}}{r^2 f_h}$ and $F_{Df} = \frac{C_{Df}}{r^2 f_v}$ where C_{Th} and C_{Df} are inverse square force constants for thermophoresis and diffusiophoresis, $C_{Th} = f_h F_{Th} r^2$ and $C_{Df} = f_v F_{Df} r^2$. The inverse square force constants C for the thermophoretic force and the diffusiophoretic force can be formulated as (Wang et al., 1978)

$$C_{Th} = -\frac{3\pi\mu_a d_p (k_a + 2.5k_p Kn) k_a D_d (T_a - T_s) f_h}{5(1 + 3Kn)(k_p + 2k_a + 5k_p Kn) \rho} \quad (14)$$

$$C_{Df} = -\frac{3\pi\mu_a D_d (0.74) D_w M_a d_p (\rho_{v,a} - \rho_{v,s}) f_v}{2(1 + \alpha Kn) M_w \rho_a} \quad (15)$$

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If electric forces are approximated by inverse square forces (repulsive for like charges, attractive for unlike charges and neglecting image charges), the inverse square force constant for electrical forces is (Tinsley, 2010)

$$C_{EI} = \frac{Qq}{4\pi\epsilon_0} \quad (16)$$

5 Using the relationship between collision efficiency and collision kernel, an effective collision efficiency can be derived from the forces. The collision kernel K for each force constant C can be calculated as (Ladino et al., 2011b)

$$K = \frac{4\pi B_p C}{\exp\left(\frac{2B_p C}{D_{diff} f_p d_p}\right) - 1} \quad (17)$$

10 where B_p is the mobility of particles. From the collision kernel, the different collision efficiencies for each mechanism can be calculated using the relationship

$$E = \frac{4K}{\pi(D_d + d_p)^2(U(D_d) - u(d_p))} \quad (18)$$

3 Experimental setup

3.1 Instrumentation

15 Our collision nucleation chamber (CLINCH) is similar to the one used by Ladino et al. (2011b) for contact freezing studies with some modifications to observe the frozen fraction of droplets at different times. It is a continuous flow chamber which consists of two parallel plates separated by 1 cm width with side windows for the detector. Both chamber walls are held at the same temperature and are covered with ice, leading to an environment that is saturated with respect to ice and subsaturated with respect to

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ods. We chose to determine the charge by passing the droplet stream through a capacitor consisting of two parallel plates which were connected to a DC voltage supply. The droplet generator was placed exactly at the top edge of the plates. These two plates were kept at 6 mm distance from each other and a DC voltage was applied. Due to the presence of the charge on the droplets, the droplets were either deflected toward the positively or negatively charged plate. Multiple measurements were performed at different times in order to obtain the average charge on the particles. The charge on the droplets varied from 0.16 fC (1000 e) to 80 fC (50 000 e). The charge on the droplet remained the same once the droplet generator was turned on but could shift to a different value when the droplet stream was turned off and turned on again. The mean charge on the droplets was about 65 fC ($39\,000\text{ e} \pm 20\,000\text{ e}$).

3.4 Experimental procedure

The collision ice nucleation experiments were conducted at temperatures between 261 and 236 K. Initially the chamber was evacuated for 5 min and then cooled to 258 K. To cover the walls with a thin layer of ice the chamber was filled with distilled water for 10 s and then flushed out. The chamber was again evacuated for 3 min and the detector was mounted. When the desired temperature of the chamber was reached, the droplet generator was turned on and droplets were observed in the detector. This blank experiment without aerosol particles was performed at each temperature in order to ensure that there is no droplet freezing without particles. After the blank experiments, the aerosol flow was turned on and the actual experiment was performed. After completing the experiment for one temperature, the temperature of the chamber was lowered in steps of 2 to 3 K until the homogeneous freezing temperature was reached.

4 Experimental results

Figure 1 shows the frozen fraction of droplets as a function of temperature for the investigated concentrations of the 200 nm silver iodide particles and residence times of 2 s (panel a) and 4 s (panel b). Error bars shown represent an uncertainty in the frozen fraction due to the classification (liquid or ice) uncertainty originating from the measurement errors of the IODE detector (Lüönd et al., 2010). As the chamber temperature was decreased the frozen fraction started to rise and after reaching a certain value it remained constant. The frozen fraction plateau is reached at about 245 K. A frozen fraction of 1 is not reached even for the lowest investigated temperature of 238 K. According to classical nucleation theory, homogeneous nucleation becomes effective only for $T < 238$ K (e.g. Ickes et al., 2014). We assume that for $T < 245$ K heterogeneous freezing on AgI particles is so efficient that each collision of a particle with a droplet leads to the immediate freezing of the droplet (freezing efficiency of 1) and the frozen fraction plateau is reached. For $T > 245$ K, the probability of droplet freezing is < 1 , and the collision of a particle with a droplet does not necessarily induce freezing. For $T < 245$ K, frozen fractions increase with increasing particle concentration from 500 to 5000 cm^{-3} without reaching a value of 1 and they are higher for 4 s residence time than for 2 s residence time. This is in accordance with immediate contact freezing once the droplet has collected a particle. This limits the contact freezing by the probability that a droplet actually captures a particle while it is falling through the chamber. If the freezing probability for $T < 245$ K is assumed to be 1, this temperature range can be used to deduce collision efficiencies from our experimental data. We therefore define data points that correspond to unity freezing probability and use them to derive experimental collision efficiencies. These points are indicated by open symbols in black rectangles in Fig. 1. Figure 2, shows the evolution of the frozen fraction as a function of the residence time in the chamber calculated as

$$FF = 1 - e^{-E_{\text{exp}}K_{\text{geo}}C_{\text{par}}t} \quad (19)$$

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where K_{geo} is the geometrical area swept out by the droplet per unit time t . C_{par} is the particle concentration and E_{exp} is the collision efficiency that fits to the experimental results best. Since the collision efficiency should be the same for all concentrations and not depend on residence time, E_{exp} was determined by simultaneously minimizing the difference between the mean values of frozen fraction indicated by the symbols in Fig. 2 and the frozen fraction calculated with Eq. (19). This yielded a value of $E_{\text{exp}} = 0.13$ in reasonable agreement with all data points taking experimental uncertainties into account. To show the sensitivity of the frozen fraction to the assumed collision efficiency, curves for $E = 0.02$ (according to Fig. 6) are also given in Fig. 2 (as dashed lines).

5 Comparison of the different formulations of collision efficiency

To compare the experimentally derived collision efficiency of $E = 0.13$ with total collision efficiencies calculated with the theoretical expressions of Sect. 2, we will calculate collision efficiencies for an AgI aerosol by water droplets falling through the 80 cm CLINCH chamber which is held at ice saturation at 261 K. Temperature and vapor pressure gradients between the droplet surface and the surrounding are calculated as well as the slow evaporation of the droplet along its path through the chamber in time increments of 0.01 s. Mean collision efficiencies for the whole chamber length are obtained by averaging over the individual 0.01 s increments. In this simulation, the droplet has a diameter of 80 μm when it enters the chamber and shrinks to 79 μm at the end of the chamber. This slow evaporation induces a temperature gradient between the surrounding and the droplet ($T_{\text{a}} - T_{\text{s}} = 0.3$ K) leading to thermophoresis. AgI particles have a density of 5600 kg m^{-3} and one elemental charge since they passed through a DMA for size selection. Major uncertainties are associated with the charge of the droplets. For the calculations shown in Fig. 3, a charge of 50 000 e of opposite sign to that of the particles was assumed. Figure 3a shows the collision efficiencies of Brownian diffusion, interception and impaction for the formulations P05 described in Sect. 2.2.1 and S83

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by impaction for diameters $> 2 \mu\text{m}$. In this range Brownian diffusion, electrophoresis and thermophoresis contribute significantly to the total collision efficiency. For 200 nm particles, the total collision efficiency is lowest (0.01) for the combination P05 and A06 and highest (0.02) for the combination S83 and W78. In our approach total collision efficiencies are obtained by adding up collision efficiencies of the different processes with values ≥ 0 . Negative collision efficiencies were not considered since they lack physical meaning. In trajectory calculations (Tinsley, 2010; Tinsley and Leddon, 2013) the simultaneous action of the different forces on the particle can be investigated. These calculations show that e.g. for small particles, the total collision efficiency can be lower than the one by Brownian diffusion alone when Brownian diffusion is diverted by repulsion of particles carrying charges of the same sign as the droplet (Tinsley et al., 2006).

6 Comparison with previous experimental work

A direct comparison of our experimental results with other measurements of collision efficiencies is not possible because collision efficiency is sensitive to many parameters, which are only partly the same in different experiments. Important parameters that determine the collision efficiency are droplet and particle sizes, charges on droplets and particles, relative humidity and temperature. Laboratory studies summarized by Wang and Pruppacher (1977) and Ladino et al. (2011b) have all been performed at or close to room temperature. In a critical review, Wang and Pruppacher (1977) criticize most older studies for insufficient control of relative humidity, insufficient control or knowledge of charges on droplets and particles, and the use of large droplets so that the terminal velocity is not reached during the experiment. In the following, the relevant studies to compare with our data are summarized. Lai et al. (1978) investigated collection efficiency of AgCl aerosol particles by freely falling water droplets in nitrogen. For 300, 500, and 900 nm diameter particles scavenged by 1.24 mm diameter droplets, they measured collection efficiencies of 0.107, 0.016 and 0.045, respectively. These results

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in the experiment of Wang and Pruppacher (1977). Ladino et al. (2011b) determined collision efficiencies for aerosol particles scavenged by cloud droplets in CLINCH using 26 μm diameter droplets. They exposed freely falling water droplets at 298 K and 90 % RH to an aerosol consisting of lithium metaborate particles with diameters between 0.1 and 0.66 μm and observed collision efficiencies between $E = 0.08$ –1.75. $E_{\text{tot}} > 1$ are obtained because of the high efficiency of Brownian diffusion for small particles. Figure 7 shows that their experimental results are in general agreement with the theoretical predictions. Ardon-Dryer et al. (2015) determined collision efficiencies between Polystyrene Latex Spheres (PSL) with radii from 0.125–0.475 μm and 43 μm diameter droplets charged with $400 \pm 40 e$. Collision efficiencies ranged from 5.7×10^{-3} to 8.6×10^{-3} for RH = 15 % and from 6.4×10^{-3} to 2.2×10^{-2} at 88 % RH. These values are lower than the ones reached in this study which may be explained by the lower charge on the PSL spheres.

7 Discussion

7.1 Discrepancies between theoretical and experimentally derived collision efficiencies

The experimentally derived collision efficiencies are almost one order of magnitude higher than the theoretical ones. It is unlikely that the experimentally derived ones are by this amount too high. The assumption that every collision leads to droplet freezing can only result in too high collision efficiencies. A conceivable process that would result in an overestimation of the collision efficiency could be that droplet freezing would influence the velocity of the droplets in such a way that frozen droplets collide with liquid ones. However, considering the sequence of frozen and liquid droplets, such a bias does not seem to exist. Brownian diffusion is the main collision mechanism for small particles in the absence of charges and one of the dominating contributions to the total collision efficiencies for the 200 nm diameter particles investigated in this

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Table 1. List of symbols.

B_p	Mobility of particles (s kg^{-1})	C_c	Cunningham slip correction (unitless)
C_{Df}	Force constant for ventilated diffusiophoresis ($\text{kg m}^3 \text{s}^{-2}$)	C_{Ei}	Force constant for electrophoresis ($\text{kg m}^3 \text{s}^{-2}$)
C_{Th}	Force constant for ventilated thermophoresis ($\text{kg m}^3 \text{s}^{-2}$)	C_p	Specific heat capacity of air ($1005 \text{ kJ kg}^{-1} \text{ K}$)
D_{diff}	Diffusion coefficient of aerosol particles ($\text{m}^2 \text{s}^{-1}$)	D_d	Diameter of the droplet (m)
d_p	Diameter of the particle (m)	D_w	Diffusivity of water vapor ($\text{m}^2 \text{s}^{-1}$)
E	Collision efficiency	E_{Tot}	Sum of all contributing mechanisms of collision efficiency
E_{Br}	Collision efficiency due to Brownian diffusion	E_{int}	Collision efficiency due to interception
E_{imp}	Collision efficiency due to impaction	E_{Th}	Collision efficiency due to thermophoresis
E_{Df}	Collision efficiency due to diffusiophoresis	E_{Ei}	Collision efficiency due to electrophoresis
k_a	Thermal conductivity of air ($\text{J m}^{-1} \text{s}^{-1} \text{K}^{-1}$)	k_p	Thermal conductivity of particle ($0.419 \text{ J m}^{-1} \text{s}^{-1} \text{K}^{-1}$)
k_B	Boltzmann constant ($\text{kg m}^2 \text{s}^2 \text{K}^{-1}$)	P_e	Peclet number
P_r	Prandtl number for air	p_s^0	Saturation vapor pressure at droplet surface
p_a^0	Saturation vapor pressure of environment	R	Diameter ratio between particle and droplet
Re	Reynolds number	Sc	Schmidt number of aerosol particles
Sc_w	Schmidt number for water vapor air	St	Stokes number (S83)
Stk	Stokes number (P05)	St^*	Critical stokes number
T	absolute temperature (K)	T_a	Air temperature (K)
T_c	Air temperature in Celsius	T_s	Temperature of droplet surface (K)
U	Terminal velocity of droplet (m s^{-1})	u	Terminal velocity of particle (m s^{-1})

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Table 2. Greek or Latin letters.

α	Packing density i.e. water volume present in unit volume of air	σ	Viscosity ratio of water to air
μ_a	Dynamic viscosity of air ($\text{kg m}^{-1} \text{s}^{-1}$)	μ_w	Viscosity of water at 273 K ($1.787 \times 10^{-3} \text{ kg m}^{-1} \text{s}^{-1}$)
ρ_a	Density of air (1.293 kg m^{-3})	ρ_w	Density of water (1000 kg m^{-3})
ρ_p	Density of aerosol particles (for AgI: 5600 kg m^{-3})	τ	Relaxation time (s)
λ_a	Mean free path of air molecules (m)		

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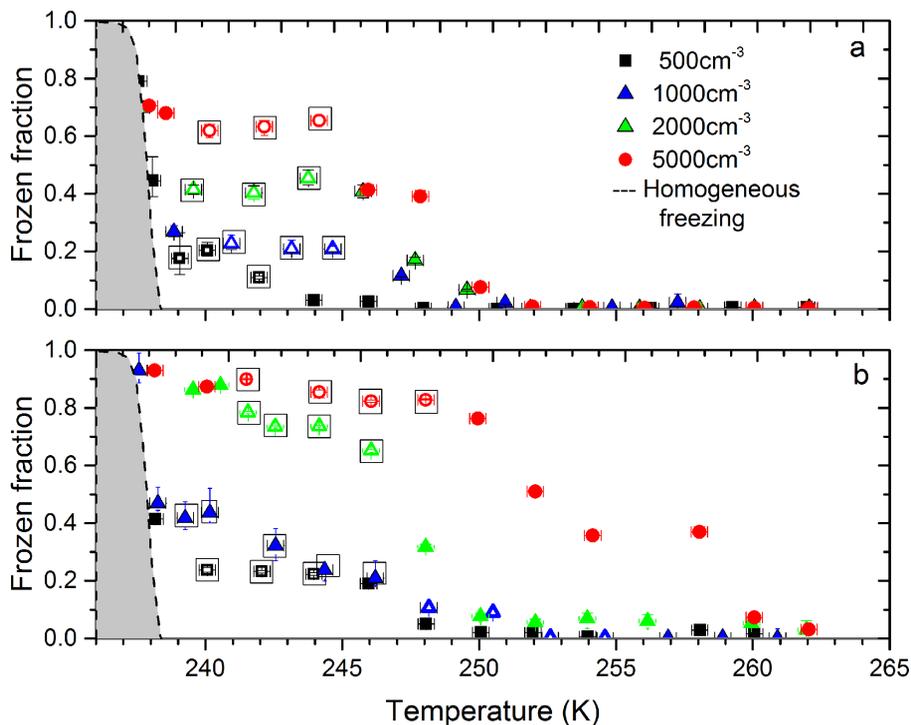


Figure 1. Frozen fraction against chamber temperature for a droplet residence time of 2 s **(a)** and for a droplet residence time of 4 s **(b)** for different concentrations of silver iodide. The dashed line and gray shaded area indicate homogeneous freezing from blank experiments. Open symbols in the black rectangles refer to the experiments used for the calculation of collision efficiencies.

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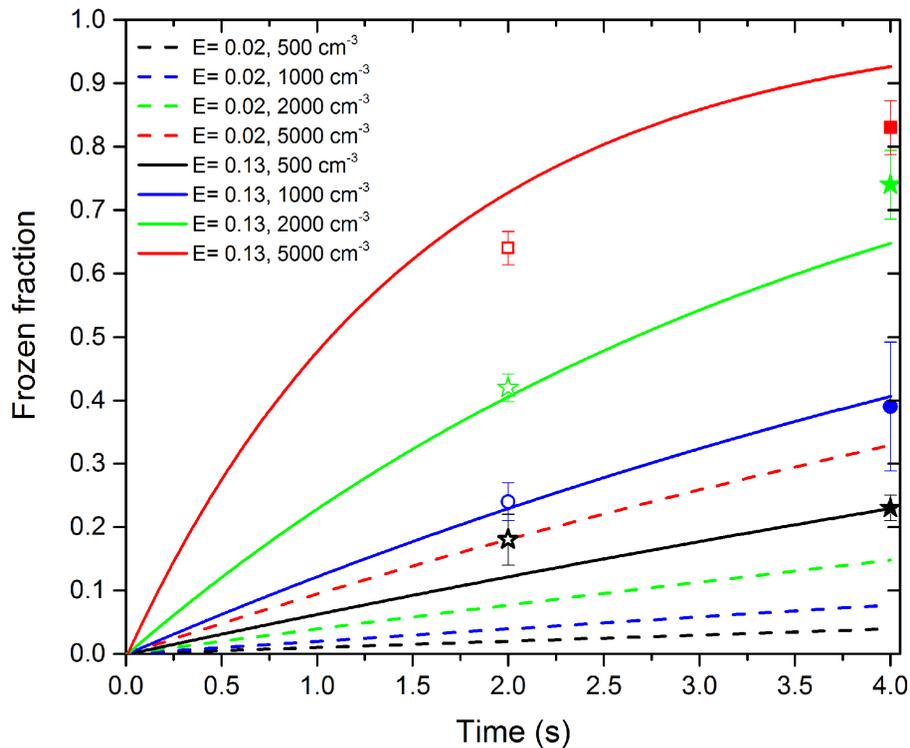


Figure 2. Evolution of the frozen fraction as a function of the residence time in the chamber calculated with Eq. (19) for the different particle concentrations from 500 to 5000 cm^{-3} . Solid lines are calculated assuming a collision efficiency $E_{\text{exp}} = 0.13$, dashed lines for $E = 0.02$. Symbols and uncertainty bars give the average and SD of the frozen fraction plateau values indicated by open symbols in Fig. 1.

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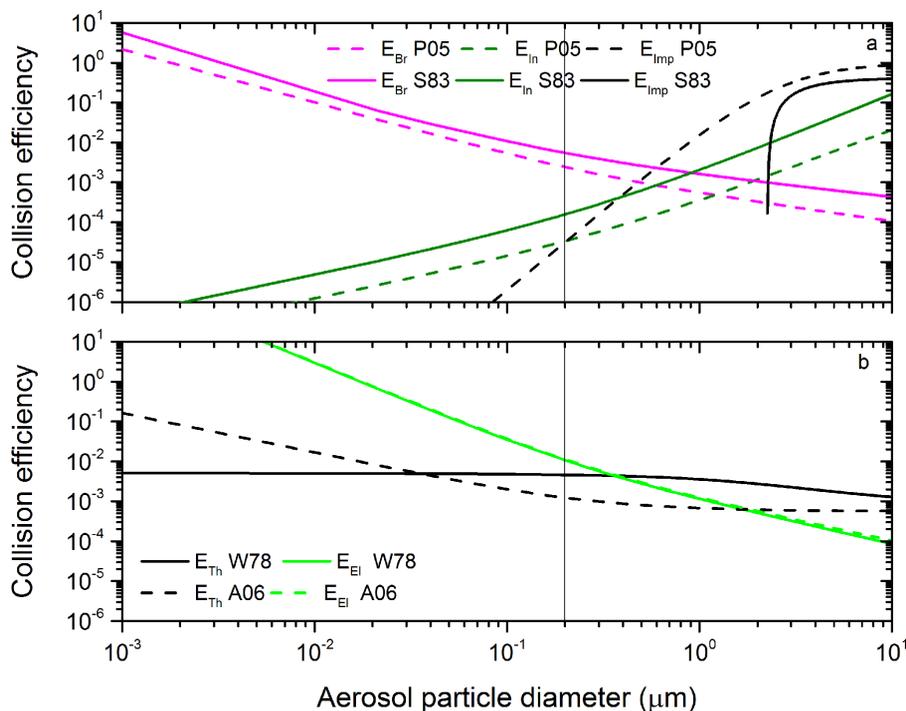


Figure 3. Calculated collision efficiency for a droplet of 80 μm diameter as a function of aerosol particle diameter at a temperature of 261 K and ice saturation. The contributions of Brownian motion, interception and impaction are shown in (a) for the formulations by Park et al. (2005) (P05) and Slinn (1983) (S83). The contributions for thermophoresis, diffusiophoresis and electrophoresis are shown in (b) for the formulations by Andronache et al. (2006) (A06) and Wang et al. (1978) (W78). The gray vertical line indicates the 200 nm diameter particles used in the experiments.

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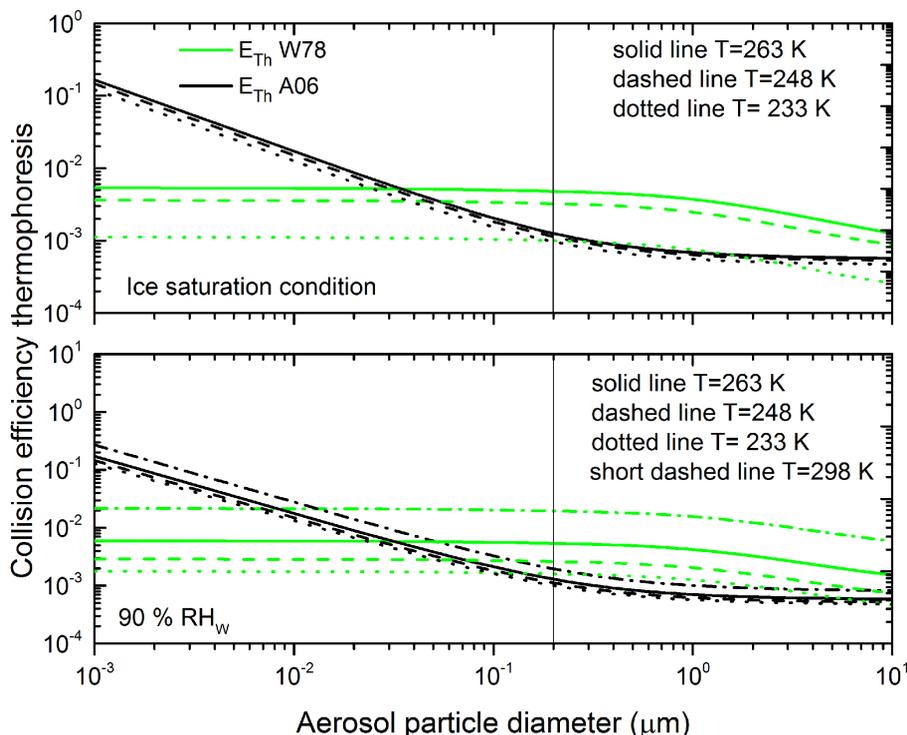


Figure 4. Dependence of thermophoresis on aerosol particle diameter. **(a)** following Anronache et al. (2006) (A06) and Wang et al. (1978) (W78) for a droplet of $80 \mu\text{m}$ diameter at ice saturation for temperatures of 263, 248 and 233 K. **(b)** shows the dependence of the collision efficiency due to thermophoresis for the same temperatures at 90 % relative humidity with respect to water. The gray vertical line indicates the 200 nm diameter particles used in the experiments.

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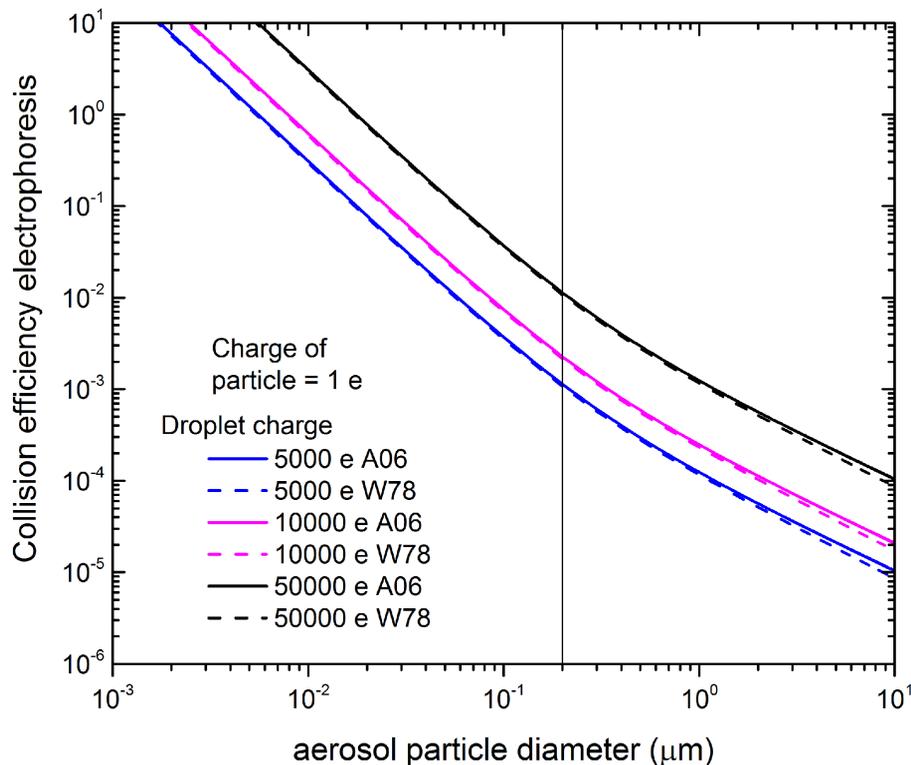


Figure 5. Dependence of electrophoresis on droplet charges for the formulations of Antronache et al. (2006) (A06) and Wang et al. (1978) (W78). The legend indicates the elementary charge on the droplets. The aerosol particles carry one elementary charge. The gray vertical line indicates the particle diameter of our experiments.

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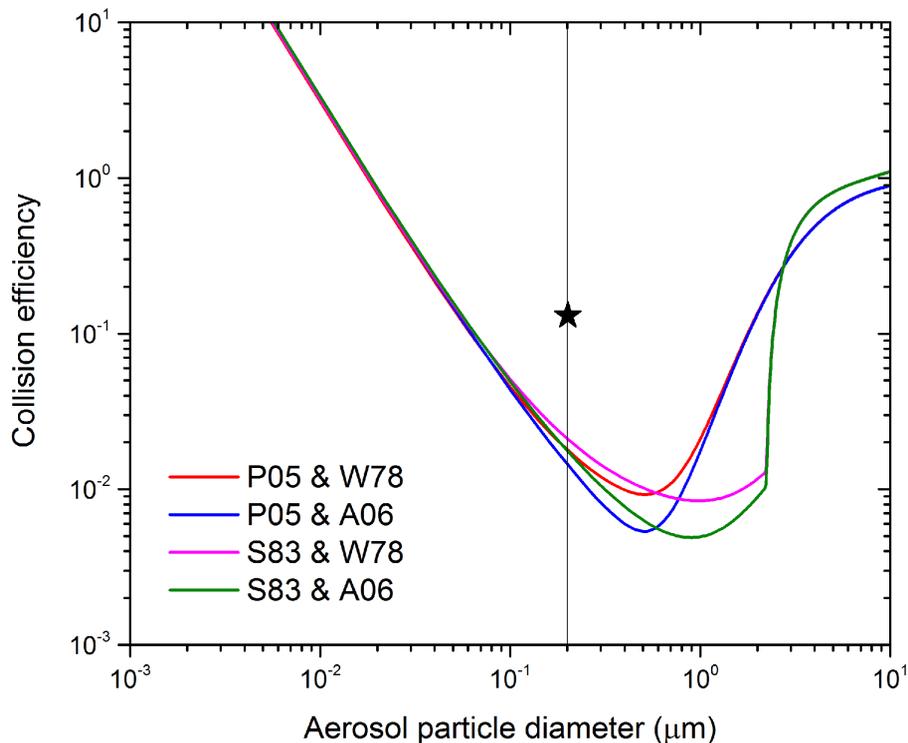


Figure 6. Total collision efficiency for a droplet of 80 μm diameter as a function of aerosol particle diameter at a temperature of 261 K and ice saturation. The total collision efficiency is the sum of all individual contributors. The vertical line indicates the particle size used in our experiment. The experimentally determined collision efficiency for 200 nm silver iodide particles colliding with 80 μm water droplets is shown as black star.

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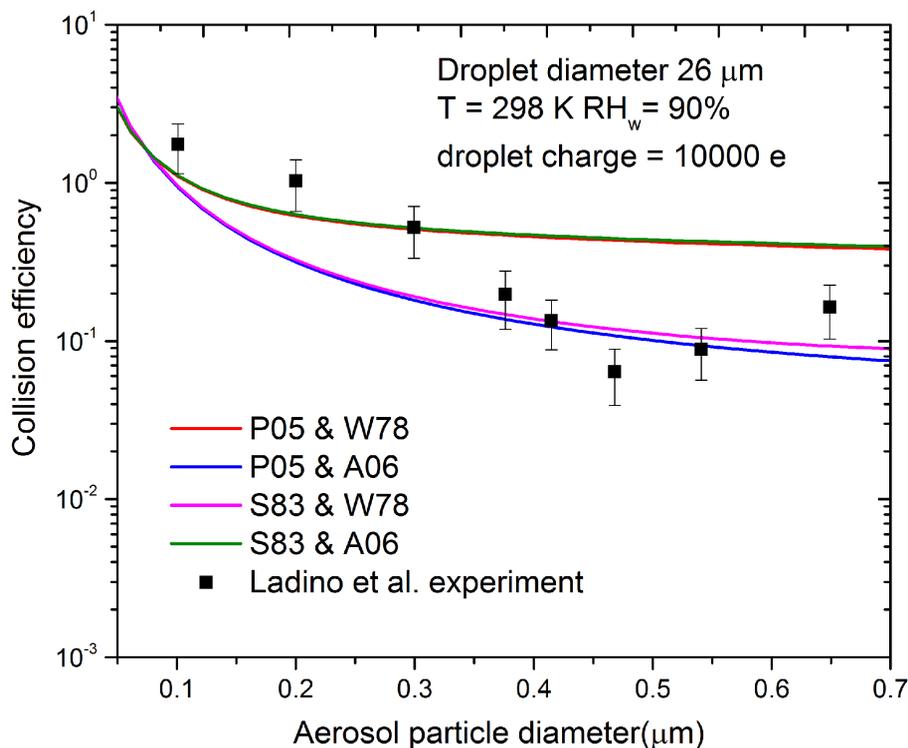


Figure 7. Total collision efficiency for a droplet of 26 μm diameter as a function of aerosol particle diameters at a temperature of 298 K and 90 % relative humidity with respect to water. The black squares indicate the measured collision efficiency.

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