



Uptake of HO₂ radicals on Arizona test dust surface

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Uptake of HO₂ radicals on Arizona test dust surface

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Abstract

The interaction of HO₂ radicals with solid films of Arizona Test Dust (ATD) was studied using a low pressure flow reactor (1–9 Torr) combined with a modulated molecular beam mass spectrometer for monitoring of the gaseous species involved.

The reactive uptake coefficient of HO₂ was measured from the kinetics of HO₂ consumption on Pyrex rods coated with ATD as a function of HO₂ concentration ($(0.35\text{--}3.30) \times 10^{12}$ molecule cm⁻³), relative humidity (RH = 0.02–94 %), temperature ($T = 275\text{--}320$ K) and UV irradiance intensity ($J_{\text{NO}_2} = 0\text{--}0.012$ s⁻¹). The initial uptake coefficient was found to be independent of concentration of HO₂, temperature and irradiation conditions, and to decrease with increasing relative humidity: $\gamma_0 = 1.2/(18.7 + \text{RH}^{1.1})$ (calculated using geometric surface area, with 30 % estimated conservative uncertainty). An upper limit of 5 % was found for the H₂O₂ forming pathway of the HO₂ reaction with ATD surface. The results of the measurements indicate that HO₂ loss on dust aerosol may be a non negligible sink for HO_x species in the troposphere with the effect depending on specific local conditions.

1 Introduction

The HO₂ radical is an important atmospheric species, which controls the oxidative capacity of the troposphere through rapid interconversion between HO_x (OH, HO₂) species. HO₂ is a precursor of the tropospheric ozone through its reaction with NO and further photodissociation of NO₂, resulting in production of ozone in the presence of oxygen (Finlayson-Pitts and Pitts, 2000). The HO₂ radical is also involved in HO_x and halogen catalyzed cycles of stratospheric ozone depletion (Bedjanian and Poulet, 2003).

The atmospheric concentration of HO_x family is controlled by the production and loss rates of these species. While the chemistry of HO_x in the gas phase is, in general, well understood, the lack of reliable data on heterogeneous loss of HO₂ and the

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strong need for such data are more and more frequently mentioned in the literature (Thornton et al., 2008; Mao et al., 2010; Macintyre and Evans, 2011). The information on kinetics and mechanism of the interaction of HO_x with different surfaces of atmospheric relevance is essential to accurate modelling of the chemical composition and prediction of changes in the oxidative capacity of the troposphere and regional air quality. Numerous previous studies have consistently reported a discrepancy between modelled and observed concentrations of HO₂ in different regions. The overestimation of HO₂ concentrations by the models was attributed to heterogeneous loss of these radicals on aerosol surface as a missing HO₂ sink, not properly accounted for in the models (Cantrell et al., 1996a,b; Jaeglé et al., 2000; Kanaya et al., 2000; Sommariva et al., 2004, 2006; De Reus et al., 2005; Mao et al., 2010). The laboratory database for uptake coefficients of HO₂ on different surface types is rather scarce, especially for solid surfaces. For example, only one direct study is available for HO₂ uptake on soot (Bedjanian et al., 2005) and no data have been reported so far for the interaction of HO₂ with mineral dust surfaces. In a few studies, attempts were made to summarize the available uptake data and parameterize them for further use in atmospheric modelling (Jacob, 2000; Thornton et al., 2008; Macintyre and Evans, 2011). Thus, recently, Macintyre and Evans (2011) reviewed the existing laboratory data on HO₂ uptake on tropospheric aerosol and derived the global mean uptake coefficient of HO₂, $\gamma = 0.028$, which is by an order of magnitude lower than those considered in earlier works (Jacob, 2000; Thornton et al., 2008). Another critical issue concerning the heterogeneous interaction of HO₂ with atmospheric aerosol is the reaction mechanism, especially with regard to the formation of H₂O₂ as the reaction product. Depending on whether or not H₂O₂ is produced, the HO₂ uptake on aerosols has opposite effects on the concentration of H₂O₂. The only product study of HO₂ interaction with solid surface is that of Loukhovitskaya et al. (2009), where H₂O₂ was identified as the main product of the HO₂ reaction with a solid salt surface.

Considering the limited kinetic and mechanistic data on HO₂-aerosol interaction and that heterogeneous reactions of HO₂ still remain a significant source of uncertainty

in atmospheric modelling of HO_x budget, it is clear that additional laboratory studies of HO₂ uptake, including product study as well as temperature and relative humidity dependence, on various aerosol types are strongly required. In the present study we report the measurements of the uptake coefficient of HO₂ radicals on Arizona Test Dust (ATD), mimicking the mineral atmospheric aerosol, under dark and UV irradiation conditions as a function of relative humidity and temperature. The possible formation of H₂O₂ as a reaction product is also examined.

2 Experimental

2.1 Preparation of ATD films

Solid films of ATD were deposited on the outer surface of a Pyrex tube (0.9 cm o.d.) using suspension of ATD (Powder Technology Inc., nominal 0–3 μm ATD) in ethanol. Prior to film deposition, the Pyrex tube was treated with hydrofluoric acid and washed with distilled water and ethanol. Then the tube was immersed into the suspension, withdrawn and dried with a fan heater. As a result, rather homogeneous (to eye) solid films were formed at the Pyrex surface. In order to eliminate the possible residual traces of ethanol, prior to uptake experiments, the freshly prepared ATD samples were heated at (100–150) °C during (20–30) min under pumping. In order to measure the mass of the sample on the Pyrex tube the deposited solid film was mechanically removed at the end of the kinetic experiments. BET surface area of the ATD powder was determined using a Quantachrome – Autosorb -1-MP-6 apparatus and nitrogen as adsorbate gas and was found to be $85 \pm 10 \text{ m}^2 \text{ g}^{-1}$.

2.2 Flow reactor

The interaction of HO₂ with solid ATD films was studied at 1–9 Torr total pressure of He (used as a carrier gas) in a discharge flow reactor with mass spectrometric detection of the gaseous species involved. The experimental equipment and approach used for the

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kinetic measurements were described in previous papers from this group (Bedjanian et al., 2005; Loukhovitskaya et al., 2009; El Zein and Bedjanian, 2012). The main reactor (Fig. 1) consisted of a Pyrex tube (40 cm length and 2.4 cm i.d.) with a jacket for the thermostatted liquid circulation. Experiments were carried out using a coaxial configuration of the flow reactor with movable central injector: the Pyrex tube with deposited sample was introduced into the main reactor along its axis. The coated tube could be moved relative to the outer tube of the injector that allowed the variation of the solid film length exposed to gas phase reactant and consequently of the reaction time. The walls of the main reactor as well as of the outer tube of the movable injector (in contact with HO₂) were coated with halocarbon wax in order to minimize the heterogeneous loss of HO₂ outside the reaction zone.

Externally, the reactor was surrounded by 6 UV lamps (Sylvania BL350, 8 W) with a broad UV emission spectrum between 315–400 nm. The UV lamps were installed into an aluminum light-tight box covering the main reactor tube. Therefore, by switching on or off the lamps, the kinetic measurements could be realized under UV irradiation or dark conditions, respectively. The irradiance intensity in the reactor was characterized by direct measurements of the NO₂ photolysis frequency, J_{NO_2} , as a function of the number of lamps switched on. The values of J_{NO_2} were found to be between 0.002 and 0.012 s⁻¹ for 1 to 6 lamps switched on, respectively (El Zein and Bedjanian, 2012).

2.3 Generation of HO₂ radicals and measurement of absolute concentrations

Two methods were used to produce HO₂ radicals. In the first one, HO₂ radicals were formed in the fast reaction of fluorine atoms, produced in the microwave discharge of F₂/He mixture, with excess H₂O₂:



It was verified by mass spectrometry that more than 90 % of F₂ was dissociated in the microwave discharge. Initial concentrations of F₂ and H₂O₂ were ~ 10¹² and ~ 10¹⁴ molecule cm⁻³, respectively. To reduce F atom reactions with glass surface

inside the microwave cavity, a ceramic (Al_2O_3) tube was inserted in this part of the discharge tube. The second source of HO_2 used in this study was the reaction of Cl atoms with an excess of CH_3OH in presence of O_2 :



Chlorine atoms were generated by microwave discharge in Cl_2 diluted with He. Initial concentration of Cl_2 was in the range $(1-3) \times 10^{12}$ molecule cm^{-3} , and the fraction of dissociated Cl_2 was around 20–30%. Methanol was introduced into the reactor from a bubbler containing thermostated ($T = 298$ K) liquid methanol. The concentrations of methanol and oxygen in the reactor were generally in the range $(1-3) \times 10^{14}$ and $(3-10) \times 10^{14}$ molecule cm^{-3} , respectively. Under these experimental conditions Reactions (R2) and (R3) were rapidly completed ensuring that chlorine atoms and CH_2OH radicals did not reach the reaction zone (in contact with dust sample).

Combination of the chemical conversion method with mass spectrometry provides a few possibilities for HO_2 detection (Bedjanian et al., 2001). HO_2 radicals may be detected at their parent peak at $m/z = 33$ (HO_2^+). This signal should be corrected for the contribution of H_2O_2 due to its fragmentation in the ion source, which was operating at 25–30 eV. These corrections could be easily done by simultaneous detection of the signals from H_2O_2 at $m/z = 33$ and 34. The contribution of H_2O_2 at $m/z = 33$ was on the order of 3% of the intensity of H_2O_2 peak at $m/z = 34$. HO_2 may also be detected by chemical conversion to NO_2 ($m/z = 46$) through reaction with NO:



Reaction (R4) leads to simultaneous production of OH radicals, which may be rapidly scavenged by Br_2 (when added simultaneously with NO) through Reaction (R5), forming HOBr (Bedjanian et al., 1999b):



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Assuming a stoichiometric conversion of HO₂ to NO₂ and OH to HOBr, one has: [HO₂] = [NO₂] = [HOBr]. Thus, in addition, HO₂ may be detected at $m/z = 96/98$ as HOBr⁺. In the present study, the HO₂ detection at $m/z = 46$ (NO₂⁺) and $m/z = 96/98$ (HOBr⁺) was preferred to the detection at its parent peak ($m/z = 33$, HO₂⁺), since the sensitivity of the mass spectrometer at these masses was higher and corresponding MS signals were free of contributions of other species and, consequently, did not require any corrections. It should be mentioned that the concentrations of HO₂ determined through [NO₂] and [HOBr] measurements were found to be in agreement within 10%. NO and Br₂, involved in titration Reactions (R4) and (R5), were introduced at relatively high concentrations ($\sim 5 \times 10^{13}$ molecule cm⁻³) at the end of the reactor through inlet located upstream of the sampling cone (Fig. 1).

Similar reactive configuration, consisting of conversion of HO₂ to NO₂ and HOBr, was also used for the determination of the absolute concentrations of HO₂ radicals. The absolute concentrations of HOBr were measured using the reaction of OH radicals with excess Br₂ (Reaction R5). In the calibration experiments OH radicals were formed through the fast reaction of H atoms with excess NO₂:



Thus, HOBr concentrations were determined from the consumed concentration of Br₂: [OH] = [HOBr] = Δ[Br₂]. The possible influence of secondary chemistry on the procedure used for the absolute calibration of HOBr signals was discussed in details in previous papers (Bedjanian et al., 1999a, 2001) and was shown to be negligible.

The concentrations of the stable gas phase species (NO, NO₂, Br₂) in the reactor were calculated from their volumetric flow rates obtained from the measurements of pressure drop of mixtures of the species with helium in calibrated volume flasks. The absolute calibration of H₂O₂ has been performed by injecting known amounts (0.5–10 μL) of the 60 wt % solution inside the flow tube reactor and recording the parent mass peak intensity of H₂O₂ at $m/z = 34$. The integrated area of the mass spectrometric signals corresponding to the known total number of H₂O₂ molecules injected into the reactor allowed the determination of the calibration factor. The concentrations

of water vapor were determined by calculating the H₂O flow rate from the total (H₂O + He) and H₂O vapor pressures in the bubbler and the measured flow rate of He through the bubbler.

3 Results

3.1 Kinetics of HO₂ loss

Figure 2 displays a typical behavior of the concentration of HO₂ radicals upon introduction of the ATD coated tube into the reaction zone (sample in). Fast initial consumption of HO₂, followed by surface deactivation resulting in a decrease of HO₂ loss rate, was observed. When the mineral sample was withdrawn from the reaction zone after exposure to HO₂ (sample out, $t \approx 86$ min), that is when HO₂ was no longer in contact with the sample surface, the concentration of HO₂ recovered rapidly to its initial value. One may note that irradiation of the ATD surface with 6 UV lamps (UV on) had no impact on the kinetics of HO₂ loss. In the present study we have measured the initial uptake coefficient of HO₂ (γ_0), because the “quasi” steady state uptake of HO₂ was found to slowly decrease with exposure time (Fig. 2) and, in addition, could be influenced by the presence of the species from the HO₂ sources. The uptake coefficient was determined as the probability of irreversible loss of the radicals per collision with dust surface:

$$\gamma = \frac{4k'}{\omega} \times \frac{V}{S} \quad (1)$$

where k' is the first order rate coefficient of HO₂ loss (s⁻¹), ω the average molecular speed (cm s⁻¹), V the volume of the reaction zone (cm³) and S the surface area of the solid sample involved in the heterogeneous reaction (cm²).

Figure 3 displays examples of HO₂ loss kinetics in heterogeneous reaction with the surface of ATD (under quasi-steady state uptake conditions on partly deactivated surface). These data were obtained by varying the length of mineral film in contact with

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HO₂, which is equivalent to varying the reaction time. The decays of HO₂ were found to be exponential (solid lines in Fig. 3) and were treated with the first-order kinetics formalism, the rate constant being determined as:

$$k'_{\text{obs}} = -\frac{d \ln([\text{HO}_2])}{dt} \quad (2)$$

5 where t is the reaction time defined by the sample length to flow velocity ratio. The values of the observed first-order rate constants, k'_{obs} , determined from the decays of HO₂ should be corrected for the diffusion limitation in the HO₂ radial transport from the volume to the reactive surface. The radial diffusion problem for the coaxial configuration of the reactor used in the present study was solved by Gershenzon and co-workers
10 (Gershenzon et al., 1994, 1995):

$$\frac{1}{k'_{\text{obs}}} = \frac{1}{k'} + \frac{R^2}{K^d(q)D_0} \times P \quad (3)$$

where k' is a true rate constant, D_0 is the diffusion coefficient of HO₂ at 1 Torr pressure (Torr cm² s⁻¹), P is the total pressure in the reactor and $K^d(q)$ is a dimensionless rate constant of radial diffusion, which is a function of sample tube radius (r) to main reactor
15 radius (R) ratio, $q = r/R = 0.375$ (for configuration used in the present study). Diffusion corrections on k'_{obs} were calculated using Eq. (3) with $D_0 = 430$ Torr cm² s⁻¹ (Bedjanian et al., 2005; Ivanov et al., 2007) at $T = 298$ K and assuming $T^{1.75}$ -dependence of the diffusion coefficient on temperature and $K^d(q) = 4.4$ (Gershenzon et al., 1995). In order to reduce rather elevated diffusion corrections on k'_{obs} due to high uptake of HO₂ on
20 ATD surface, most of experiments were carried out at relatively low pressure of 1 Torr. The diffusion corrections applied to k'_{obs} were generally between 10 and 30 %, however for a few points measured at elevated pressures (up to 9 Torr) they reached a factor as high as 1.5.

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3.2 Dependence on sample mass

Surface area involved in the heterogeneous reaction is an important parameter which is required for calculation of the uptake coefficient. In order to determine the surface area of ATD accessible to HO₂, the uptake of HO₂ was measured as a function of the thickness of ATD sample. The experiments were performed at $T = 300$ K under dry conditions. The obtained results are presented in Fig. 4, where the uptake coefficient of HO₂, calculated applying the geometric (projected) surface area of ATD sample, is shown as a function of the ATD mass deposited per unity length of the support tube. One may note that three different regimes were observed: the first one, where geometric uptake coefficient linearly increases upon increase of the sample mass (up to nearly 0.06 mg cm^{-1}), the second one (transition region, between 0.06 and nearly 1 mg cm^{-1}), where γ continues to increase slowly, and, finally, the saturation region, where the uptake coefficient is mass-independent ($> 1 \text{ mg cm}^{-1}$). The linear dependence of γ_{geom} on mass (thickness) of the reactive film is generally considered as an indication that the entire surface area of the solid sample is accessible to the gaseous reactant (Underwood et al., 2000), which implies the use of the BET surface area in the calculations of true uptake coefficient. In the present study the linear regime of the uptake coefficient was observed at relatively low masses of the ATD coating. Working with such low masses of solid samples was associated with some experimental difficulties. Firstly, by the method that we used, the measurement of the total dust masses of a few tenths of mg was problematic and associated with high uncertainties. Secondly, the reproducibility of the kinetic data observed with dust samples of low masses was rather poor. In addition, the reason for the initial linear mass dependence of γ at very low masses could also be the incomplete coverage of the support tube by dust aggregates. It is not certain that for sample mass lower than 0.06 mg cm^{-1} a coherent dust coating is provided, although no uncovered area on the support tube was observed by visual inspection. For all these reasons we have chosen a compromise solution. Uptake experiments were carried out with masses of ATD higher than 1 mg cm^{-1} (where

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geometric uptake is independent of the sample mass) and the uptake coefficient of HO₂ was calculated with geometric (projected) surface area. Thereby, the uptake coefficient of HO₂ from the present study should be considered as an upper limit. On the other hand, the lower limit of the uptake coefficient may be also estimated. So applying the BET surface area to the experimental data observed for geometric uptake coefficient at low masses (in linear regime), it turns out that the uptake coefficient calculated with total specific surface area is by a factor 40 lower than that with geometric one.

3.3 Dependence on initial concentration of HO₂

The dependence of γ on initial concentration of HO₂ radicals, varied in the range (0.35–3.3) $\times 10^{12}$ molecule cm⁻³, was measured at $T = 300$ K under dry conditions (RH = 0.03 %). The observed results are displayed in Fig. 5. The initial uptake coefficient of HO₂, $\gamma (\pm 2\sigma) = (6.7 \pm 0.4) \times 10^{-2}$, was found to be independent of the initial radical concentration in the range of [HO₂]₀ used. Generally, initial uptake (in case of first order kinetics) is not expected to be dependent on the gas phase concentration of the reactant since at the initial stage of the surface exposure, the active sites on the surface are not depleted or blocked and are all available for the heterogeneous reaction. One may note that good agreement exists between the results obtained for the uptake coefficient using two different methods to generate HO₂ radicals (Fig. 5). This observation seems to indicate that the presence of H₂O₂ (when F + H₂O₂ reaction is used for generation of HO₂) in the reactive system has a negligible impact, at least, on the initial uptake of HO₂ radicals on ATD surface. This was verified in additional experiments where the uptake coefficient of HO₂ was measured with concentration of H₂O₂ varied between 2×10^{13} and 2.6×10^{14} molecule cm⁻³. The values of γ measured in the presence of different concentrations of H₂O₂ in the reactor were found to be similar within uncertainty of the measurements. Similar invariance of the initial uptake coefficient was observed using the Cl + CH₃OH + O₂ system as source of HO₂ and with concentration of methanol varied in the range 3.5×10^{13} – 3.0×10^{14} molecule cm⁻³.

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3.4 Dependence on RH, temperature and UV irradiation intensity

RH dependence of the uptake coefficient was studied at $T = 275$ K, with relative humidity in the reactor being varied in the range (0.02–94) %. Rather low temperature was chosen for these experiments in order to provide reasonably high RH in the reactor with relatively low total pressures used. The results obtained for initial uptake coefficients of HO₂ on ATD surface are displayed in Fig. 6. One may note again that the uptake data obtained using different chemical systems for generation of HO₂ radicals (filled and open symbols in Fig. 6) are in agreement within the experimental uncertainty on the determination of γ (estimated to be 20–30 %).

As it may be seen in Fig. 6, the values of the uptake coefficient can be considered as RH independent under dry conditions (up to RH ~ 2 %). However, significant decrease of γ is observed when RH is further increased. The solid line in Fig. 6 represents a fit to the experimental data according to the following expression:

$$\gamma_0 = 1.2 / (18.7 + \text{RH}^{1.1})$$

This empirical equation allows describing our results in the whole RH range used with estimated conservative uncertainty of 30 %.

Temperature dependence of the uptake coefficient was measured in the temperature range (275–320) K at a fixed relative humidity of 0.04 %. The results are presented in Fig. 7. As one may note, the initial uptake coefficient was found to be independent of temperature.

Dependence of the uptake coefficient on the irradiation intensity was studied in additional experiments by switching on the different number of lamps in the reactor, from 1 to 6. This corresponds to the variation of the NO₂ photolysis frequency from 0.002 to 0.012 s⁻¹. Under these irradiance conditions we have not observed any effect of the UV irradiation on the kinetics of HO₂ loss (see Fig. 2, for example) on the ATD samples in the whole range of RH used. The measured values of γ were similar (within a few %) to those under dark conditions.

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3.5 Estimation of H₂O₂ yield

In previous study from this group, H₂O₂ was detected as a product of the HO₂ uptake on salt surface (Loukhovitskaya et al., 2009). In this work, we have examined the possible H₂O₂ formation upon interaction of HO₂ radicals with ATD surface. Experiments were carried out at P = 1 Torr total pressure, T = 300 K and under dry conditions. Reaction of Cl atoms with a large excess of CH₃OH/O₂ mixture was used as a source of HO₂ radicals. The experiment consisted in the introduction of ATD sample in the reaction zone (in contact with HO₂) and monitoring of the consumed HO₂ concentration and possibly formed H₂O₂ concentration. No changes in the relatively high (due to contribution of molecular oxygen) background signal at m/z = 34 (parent peak of H₂O₂) was observed upon heterogeneous consumption of 2.1 × 10¹² molecule cm⁻³ of HO₂. This non observation of H₂O₂ in the gas phase allowed to set an upper limit of 5 % for its yield in reaction of HO₂ with ATD surface. This upper limit of H₂O₂ yield was determined as a ratio of the concentration of H₂O₂ formed (< 9.7 × 10¹⁰ molecule cm⁻³) to the concentration of HO₂ consumed.

4 Discussion

This work reports the first measurement of the HO₂ radical uptake on mineral dust. The uptake coefficient of HO₂ on Arizona Test Dust measured in the present study decreases with relative humidity being nearly 2.6 × 10⁻² and 8.4 × 10⁻³ at RH = 20 and 80 %, respectively. The negative dependence of HO₂ uptake on ATD surface on RH may be compared with the effect of humidity on the rate of the heterogeneous loss of HO₂ on salt surfaces, for which a number of studies are available. For dry aerosol particles of NaCl, Taketani et al. (2008) observed an enhancement of the HO₂ uptake in the presence of water vapor; however, Remorov et al. (2002) reported a decrease in the probability of HO₂ uptake on NaCl upon addition of water in the reactor. In a previous work from this group (Loukhovitskaya et al., 2009), no impact of water was observed

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for the uptake of HO₂ on solid NaCl and NaBr, however, inhibiting effect of water was observed for the uptake of HO₂ on MgCl₂ × 6H₂O, which is a more hygroscopic salt (Bedjanian and Loukhovitskaya, 2011). Much higher values of the uptake coefficient compared to dry salt were systematically observed for wet particles (Taketani et al., 2008, 2009) suggesting that heterogeneous loss of HO₂ is enhanced by particles containing water. One may note that even for salt surfaces the available information on RH dependence of HO₂ uptake is controversial. The RH dependence of γ observed in the present study (decrease of the uptake coefficient upon increase of RH) points to the role of water rather as blocking the available active sites on the surface. It may be noted that the γ values measured in the present study for RH between 20 and 80 % are close to that measured for the uptake coefficient of HO₂ on water, $\gamma \geq 0.01$ (Hanson et al., 1992). This fact seems to correlate, at least qualitatively, with the available data for the adsorption of water on mineral oxides (Goodman et al., 2001; Ma et al., 2010). Indeed, it was reported that water adsorption to SiO₂, Al₂O₃, MgO, Fe₂O₃, and TiO₂ (which are components of ATD) could be well described with the Brunauer–Emmett–Teller (BET) type isotherm, with the monolayer coverage occurring between 20 and 30 % relative humidity (Goodman et al., 2001; Ma et al., 2010).

In only one previous product study of HO₂ interaction with solid surface (Loukhovitskaya et al., 2009), H₂O₂ was identified as the main product of the HO₂ reaction with surface of NaBr. Considering the measured H₂O₂ yield of nearly 0.5, Loukhovitskaya et al. (2009) proposed a two-step reaction mechanism resulting in the HO₂ recombination on the surface. The upper limit of 5 %, determined in the present study for the gaseous H₂O₂ forming channel of the HO₂ + ATD reaction, points to a different mechanism of the reactive uptake of HO₂ on mineral oxides. For example, HO₂ may react with OH groups present on the surfaces of mineral oxides leading to formation of H₂O and O₂ as final reaction products. Another point, which should be mentioned, is the rather high reactive uptake of H₂O₂ on mineral surfaces which was recently reported in a number of studies (Pradhan et al., 2010a,b; Wang et al., 2011; Romanias et al., 2012). It means that even if uptake of HO₂ on ATD partly leads to the formation of H₂O₂

as a primary product, H_2O_2 , once formed, may be further processed in heterogeneous reactions on ATD surface. Temperature dependence of the uptake coefficient measured on ATD surface is also quite different from those on salt surfaces. All temperature dependence studies of HO_2 uptake on solid salt particles report a rather strong negative temperature dependence of the uptake coefficient (Antsupov, 1988; Gratpanche et al., 1996; Remorov et al., 2002; Loukhovitskaya et al., 2009), while in the present study we have not observed any effect of temperature (for $T = 275\text{--}320\text{ K}$) on the HO_2 uptake on ATD. This seems to indicate once again the difference in the uptake mechanism on these surfaces. Let's note that the temperature independent value of γ was also reported for the uptake of HO_2 on soot surface (Bedjanian et al., 2005).

The importance of HO_2 loss in the heterogeneous reaction with atmospheric dust aerosol



may be briefly discussed. First, it should be noted that the range of γ reported in the present study is close to the global mean value of 0.028 based on recent parameterisation of the available laboratory data by Macintyre and Evans (2011), but this value is significantly lower than those adopted in earlier modeling studies. The potential atmospheric impact of Reaction (R7) may be roughly estimated by comparing its rate with that of the known loss processes of HO_x in the atmosphere. In the high NO_x regime (polluted urban troposphere) a major gas phase sink for the HO_x species is Reaction (R8) of OH radicals with NO_2



combined with the heterogeneous removal of HNO_3 . For the ratio of the rates of the Reactions (R7) and (R8) one has:

$$\frac{R_7}{R_8} = \frac{k'_7[\text{HO}_2]}{k_8[\text{OH}][\text{NO}_2]}$$

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In accordance with

$$k'_7 = \frac{\omega \gamma S}{4 V}$$

and using $\gamma = 0.02$ measured in the present study for $RH = 30\%$, dust surface loading of $\sim 10^{-6} \text{ cm}^2 \text{ cm}^{-3}$ (Zhang and Carmichael, 1999; De Reus et al., 2005) the calculated value is: $k'_7 \approx 2.2 \times 10^{-4} \text{ s}^{-1}$ (for $T = 300 \text{ K}$). Further, using the value, $k_8 \sim 10^{-11} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ (Sander et al., 2011) and a typical ratio $[\text{HO}_2]/[\text{OH}] \sim 100$, we obtain: $R_7/R_8 = 2.2 \times 10^9/[\text{NO}_2]$. This ratio indicates that for concentrations of NO_2 of a few ppbv heterogeneous loss of HO_2 does not represent a significant sink for HO_x compared with Reaction (R8). However, under specific conditions, for example, of severe dust storm, when aerosol surface loading can be as high as $2 \times 10^{-5} \text{ cm}^2 \text{ cm}^{-3}$ (Zhang and Carmichael, 1999) the rate of Reaction (R7) may be comparable with that of the $\text{OH} + \text{NO}_2$ reaction.

Under low NO_x conditions (free troposphere) the loss of atmospheric HO_x is mainly due to reactions between HO_x radicals:



The rate of HO_2 loss in heterogeneous Reaction (R7) may be compared with that of self-reaction of HO_2 radicals:

$$\frac{R_7}{R_{10}} = \frac{k'_7[\text{HO}_2]}{2k_{10}[\text{HO}_2]^2} = \frac{k'_7}{2k_{10}[\text{HO}_2]}$$

One may note that the relative contribution of Reaction (R7) in this case depends on the absolute concentration of HO_2 , because the rate of the self-reaction of HO_2 is proportional to the square of the concentration of the radicals and heterogeneous reaction is first order in $[\text{HO}_2]$. With $k'_7 = (0.22\text{--}4.4) \times 10^{-3} \text{ s}^{-1}$ (calculated for aerosol surface in

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the range $(0.1\text{--}2) \times 10^{-5} \text{ cm}^2 \text{ cm}^{-3}$), $k_{10} \cong 2.5 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ (Sander et al., 2011) and typical HO₂ concentration of $\sim 10^8 \text{ molecule cm}^{-3}$, we obtain $R_7/R_{10} = 0.44\text{--}8.8$. These calculations show that heterogeneous sink for HO₂ on aerosol surface may be comparable and even higher, during severe dust storm events, than HO₂ loss through self reaction. This point is of importance not only for HO_x but also for H₂O₂ budget considering the absence of H₂O₂ in the products of HO₂ interaction with dust aerosol shown in the present study. The conclusion of these rough estimations is that HO₂ loss on dust aerosol may be a non negligible sink for HO_x species in the troposphere with an effect depending on specific conditions such as aerosol loading, relative humidity, concentrations of HO_x. It should be noted however that all the considerations above were based on the upper limit of the uptake coefficient measured on Arizona Test Dust. ATD, representing Arizona sand, mimics quite well the chemical composition of atmospheric dust, however it may differ from it in some physical and chemical properties. It is clear that additional measurements of the HO₂ interaction with real dust samples from different locations would be very useful.

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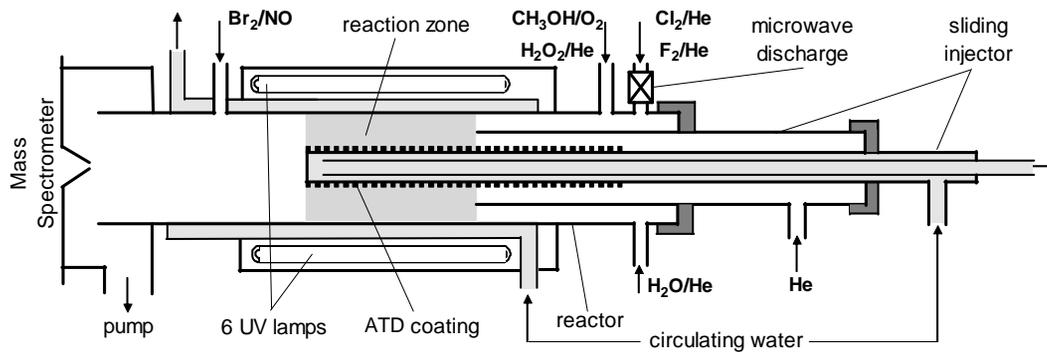


Fig. 1. Diagram of the flow photoreactor.

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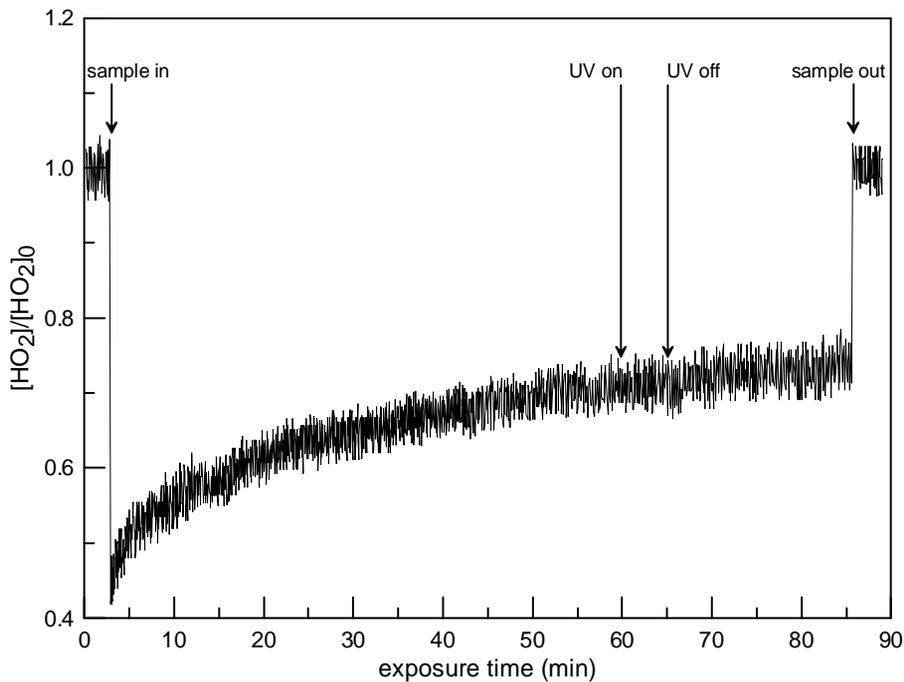


Fig. 2. Typical uptake profile of HO₂ on ATD surface: $T = 300$ K, $P = 1$ Torr, dry conditions ($RH \approx 0.02\%$), $[HO_2]_0 = 1.3 \times 10^{12}$ molecule cm^{-3} , sample mass = 0.47 mg cm^{-1} .

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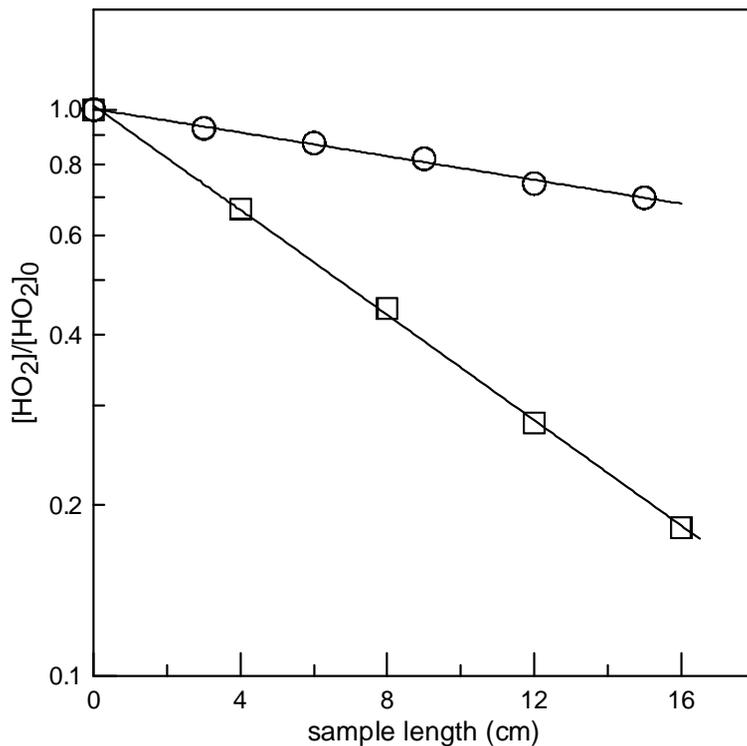


Fig. 3. Example of kinetics of HO_2 consumption in reaction with ATD surface: $T = 300\text{ K}$, $P = 1\text{ Torr}$, dry conditions, $[\text{HO}_2]_0 = 2.0 \times 10^{12}\text{ molecule cm}^{-3}$. Circles and squares correspond to the results obtained using $\text{F} + \text{H}_2\text{O}_2$ and $\text{Cl} + \text{CH}_3\text{OH} + \text{O}_2$ systems to produce HO_2 and with samples of 2.5 and 2.8 mg cm^{-1} after 75 and 20 min of exposure, respectively.

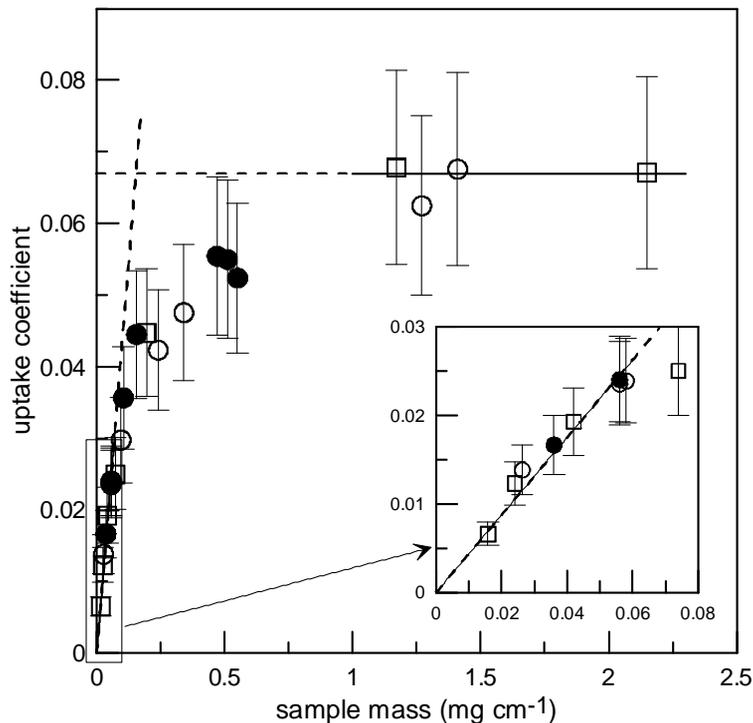


Fig. 4. Dependence of the uptake coefficients of HO₂ (calculated using geometric surface area) on mass of ATD samples (per 1 cm length of the support tube): T = 300 K, P = 1 Torr, dry conditions, [HO₂]₀ ≈ 10¹² molecule cm⁻³. Circles and squares correspond to the results obtained using F + H₂O₂ and Cl + CH₃OH + O₂ systems to produce HO₂; filled and open symbols represent the data observed with HO₂ detection at m/z = 96 (HOBr⁺) and 46 (NO₂⁺), respectively.

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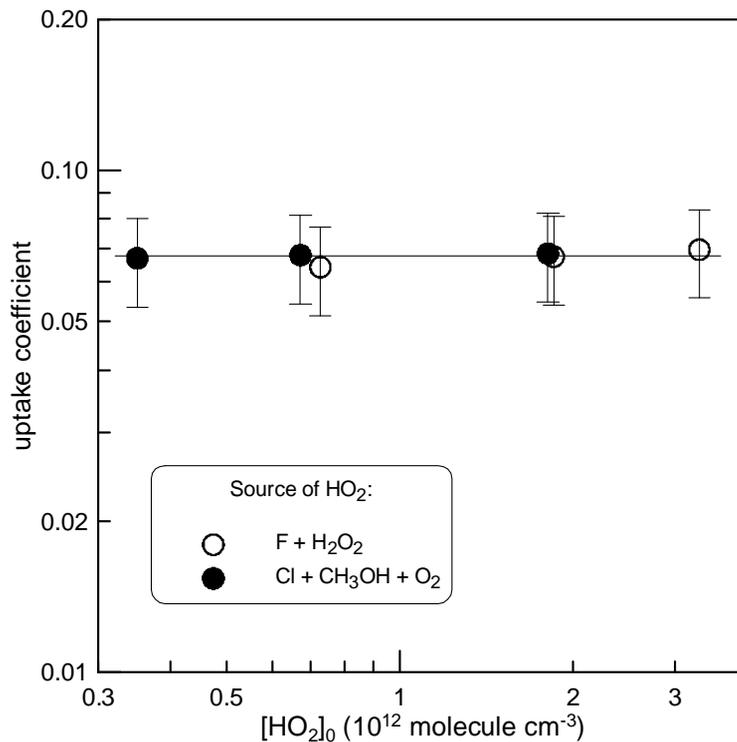


Fig. 5. Uptake coefficients as function of the initial concentration of HO₂: $T = 300$ K, $P = 1$ Torr, dry conditions, sample mass = $(1.2\text{--}1.4)$ mg cm⁻¹.

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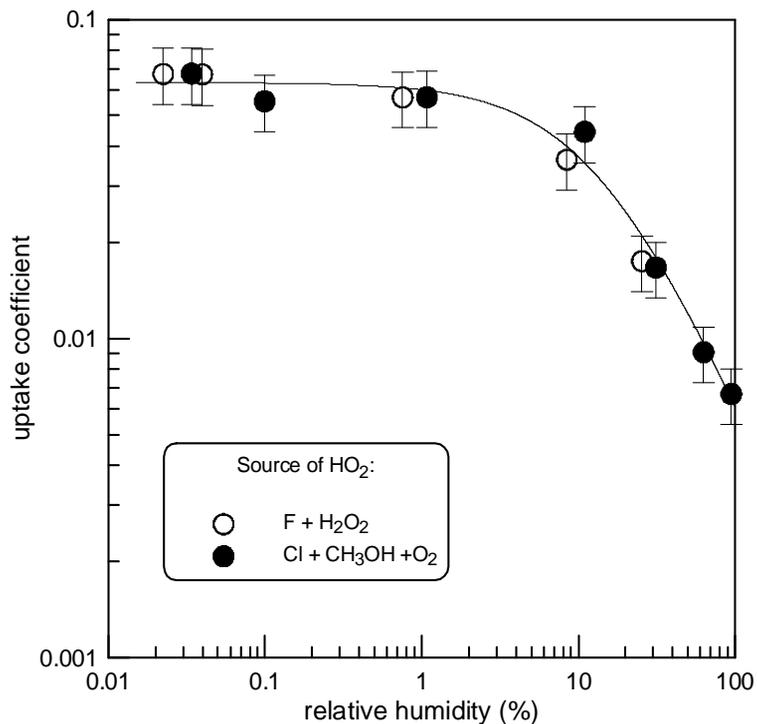


Fig. 6. Initial uptake coefficients of HO₂ on ATD as a function of relative humidity: $T = 275\text{ K}$, $P = 1.0\text{--}9.0\text{ Torr}$, $[\text{HO}_2]_0 \approx 10^{12}\text{ molecule cm}^{-3}$, sample mass = $(1.2\text{--}1.5)\text{ mg cm}^{-1}$. The data were obtained with two sources of HO₂ radicals: reactions $\text{F} + \text{H}_2\text{O}_2$ (open symbols) and $\text{Cl} + \text{CH}_3\text{OH} + \text{O}_2$ (filled symbols).

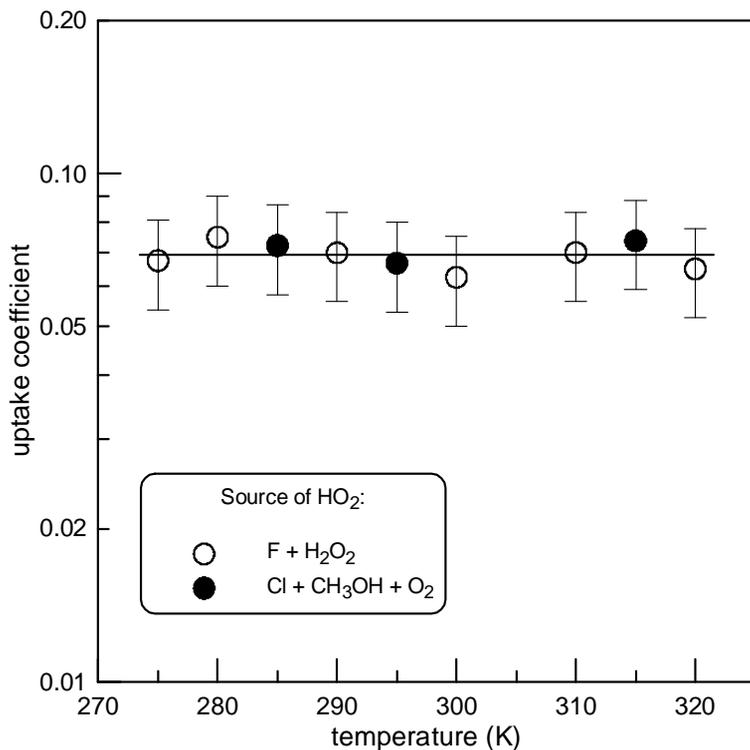


Fig. 7. Temperature dependence of the uptake coefficient of HO₂ on ATD: P = 1 Torr, T = 275–320 K, RH = 0.04 %, [HO₂]₀ ≈ 10¹² molecule cm⁻³. The data were obtained with two sources of HO₂ radicals: reactions F + H₂O₂ (open symbols) and Cl + CH₃OH + O₂ (filled symbols).

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